

Reduction of CO₂ to Chemicals and Fuels: Thermocatalysis versus Electrocatalysis

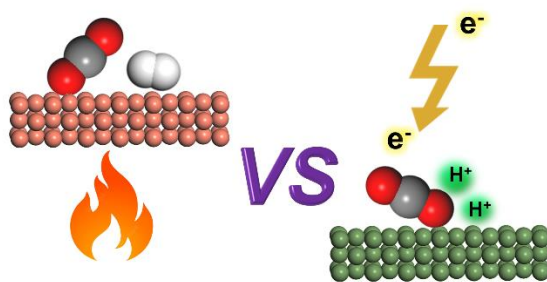
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Abstract

Reducing carbon dioxide to valuable chemicals and fuels such as formic acid, carbon monoxide, methanol, methane, ethylene, ethanol, and higher alcohol products by renewable hydrogen via thermocatalysis or by renewable electricity via electrocatalysis provides an attractive and sustainable way for achieving carbon abatement and addressing the climate change challenge. The thermocatalytic pathway is easy to scale up and realize industrial-scale applications, but some of the reactions are limited by kinetics, and / or thermodynamics equilibrium. In contrast, the electrocatalytic approach is less mature but has advantages, including low temperature and low pressure, using water as a hydrogen source, and no limitation from thermodynamic equilibrium. However, the electrocatalysis process requires the development of more effective and stable electrocatalysts. In this review, the latest progress in converting CO₂ to various chemicals or fuels via thermocatalysis and electrocatalysis is summarized and compared with an emphasis on catalysts and reaction mechanisms. The similarity and differences between thermocatalysts and electrocatalysts as well as the thermocatalytic process and electrocatalytic process are discussed in detail. The combination of strength between thermocatalysis and electrocatalysis is also introduced and discussed. Future research directions of the CO₂ conversion process are outlooked.



TOC

1. Introduction

The amount of carbon dioxide (CO₂) in the atmosphere has increased along with human emissions since the industrial revolution in the 1750s.¹ Emissions rose slowly to about 10 billion tons a year in the mid-20th century before skyrocketing to more than 35 billion tons per year in recent years.² It is estimated that about 86% of the carbon emissions come from fossil fuel (coal, oil, and natural gas) utilization, and the remaining mainly come from land utilization.³ Among the CO₂ emissions, about 46% goes to the atmosphere, 23% is dissolved in the ocean and 31% is absorbed by the land.³

CO₂ emission in the atmosphere is predicted to be closely related to climate change and global temperature increase.^{4, 5} CO₂ dissolved in the ocean will cause acidification, posing threats to the earth's ecosystems.⁶ To address the climate change issue, both efforts in CO₂ emission source control and recycling and utilization of emitted CO₂ are necessary. CO₂ emissions from the utilization of fossil fuels can be captured and further reduced to chemicals and fuels using renewable and clean energy. Utilization of CO₂ includes conversion of CO₂ to chemicals and fuels, mineralization of CO₂ for concrete building materials, etc.^{3, 7, 8} Among these processes, catalysis is an effective, economic, and sustainable approach for converting CO₂ to chemicals and fuels.^{9, 10} This technology is very attractive since it can reduce the usage of fossil fuels and provide an economic incentive to utilize CO₂. Currently, there are mainly three categories of catalytic approaches, namely, thermocatalytic, electrocatalytic, and photocatalytic ways. Thermocatalysis is typically conducted by flowing CO₂ and other gases (e.g., renewable H₂) over thermocatalysts at an increased temperatures and pressures. In contrast, the electrocatalytic process is reacting dissolved or gaseous CO₂ at the interface between electrolytes and electrodes (electrocatalysts), typically at ambient or near ambient conditions. The photocatalytic process is conducted under photo irradiation in the presence of a photocatalyst. The progress of

photocatalytic CO₂ reduction is well summarized in recent reviews,¹¹⁻¹³ so it is not discussed in this review.

So far, thermocatalytic hydrogenation of CO₂ can produce formic acid (HCOOH)/formate,¹⁴ methane (CH₄),^{15, 16} carbon monoxide (CO),¹⁷ methanol (CH₃OH),¹⁸ hydrocarbons,¹⁹ olefins²⁰, and even aromatics^{21, 22} on selected thermocatalysts, temperature, and pressure. In contrast, electrocatalytic reduction of CO₂ can also produce similar products such as HCOOH,²³ CO,²⁴ CH₄,²⁵ CH₃OH,²⁶ ethylene (C₂H₄),²⁷⁻²⁹ ethanol (C₂H₅OH),^{30, 31} and even higher products such as C₃ to C₆ hydrocarbons³² on chosen electrocatalysts, potential range, and electrolyte.

Although there are many reviews regarding CO₂ reduction via thermocatalysis^{19, 20, 33, 34} or electrocatalysis,³⁵⁻⁴⁰ there are very few reviews that summarize and compare the commonalities, similarities, and differences between these two processes together.^{41, 42} In principle, any heterogeneous reaction that involves redox or changes in oxidation states, adsorption of charged intermediates, or even heterolysis of small molecules should have parallels with electrochemical reactions occurring at electrified interfaces.⁴³ There are some catalysts that have been found both active in electrocatalysis and thermocatalysis for CO₂ reduction. For example, graphitic carbon nitride can work as a thermocatalyst, electrocatalyst, and even photocatalyst for CO₂ conversion.⁴⁴ Molybdenum sulfide, which has been widely investigated as hydrodesulfurization catalysts in thermocatalysis⁴⁵, also catalyzing the electrochemical hydrogen evolution reaction (HER)⁴⁶. In both cases, the adsorption of hydrogen atom is a crucial factor affecting the catalytic performance, while the edge sites of molybdenum sulfide are considered as the main active sites for both hydrodesulfurization reaction⁴⁷ and electrochemical HER⁴⁸. Moreover, metal nanoparticles that catalyze hydrogen peroxide (H₂O₂) synthesis by the electrochemical oxygen reduction reaction (ORR) can also work as thermocatalysts

for direct H_2O_2 synthesis via H_2 and O_2 .⁴⁹ These studies suggest that there are some commonalities between the two processes.

In this review, the conversion of CO_2 to chemicals and fuels via thermocatalysis and electrocatalysis are summarized and compared with the emphasis of catalysts and reaction mechanisms. The similarities and differences between thermocatalyst and electrocatalysts as well as the thermocatalytic and electrocatalytic processes are discussed in detail. The combination of strength between thermocatalysis and electrocatalysis, as well as future reaction directions, are also elaborated and discussed. Through this review, it is hoped that researchers in different fields can learn from each other to develop more effective catalysts and catalytic process.

2. Thermocatalysis versus Electrocatalysis

Under ordinary conditions, the occurrence of a chemical reaction is accompanied by the liberation or absorption of heat. The temperature dependence of the reaction rate constant for an elementary reaction step can be described well by the Arrhenius equation, as shown in Figure 1a. In an electrochemical reaction, the electrons and ions are also considered as reactants or products, and their potential energy can be controlled by the potential applied to the electrode (electrocatalyst). The reaction rate of an electrochemical reaction can be adjusted by temperature and overpotential applied as described by the modified Arrhenius equation shown in Figure 1b.⁵⁰ A catalyst can bind or interact with the reaction intermediates so that the intermediates can be stabilized, and the activation energy can be greatly reduced.⁵¹ From this perspective, the thermocatalysis process (Figure 1c) is similar to the electrocatalysis process (Figure 1d). In electrocatalysis, an electrolyte is needed to transfer the ions involved in the reaction process, and the reaction is typically occurred on the interface between the

electrocatalyst (electrode) and electrolyte. Therefore, electrocatalysis can be regarded as a special kind of heterogeneous catalysis. In thermocatalysis, the reaction proceeds via multiple elementary steps with various reaction intermediates. Similarly, in electrocatalysis, a series of elementary steps also happen to complete the reaction. Only one electron can be transferred in an elementary step according to the Marcus theory. In addition, pure chemical elementary steps (non-electron transfer steps) can also be involved in electrochemical reactions. The rate-determining steps in electrochemical reactions can be electron transfer steps or non-electron transfer steps (pure chemical steps, like the case in the thermocatalysis process).

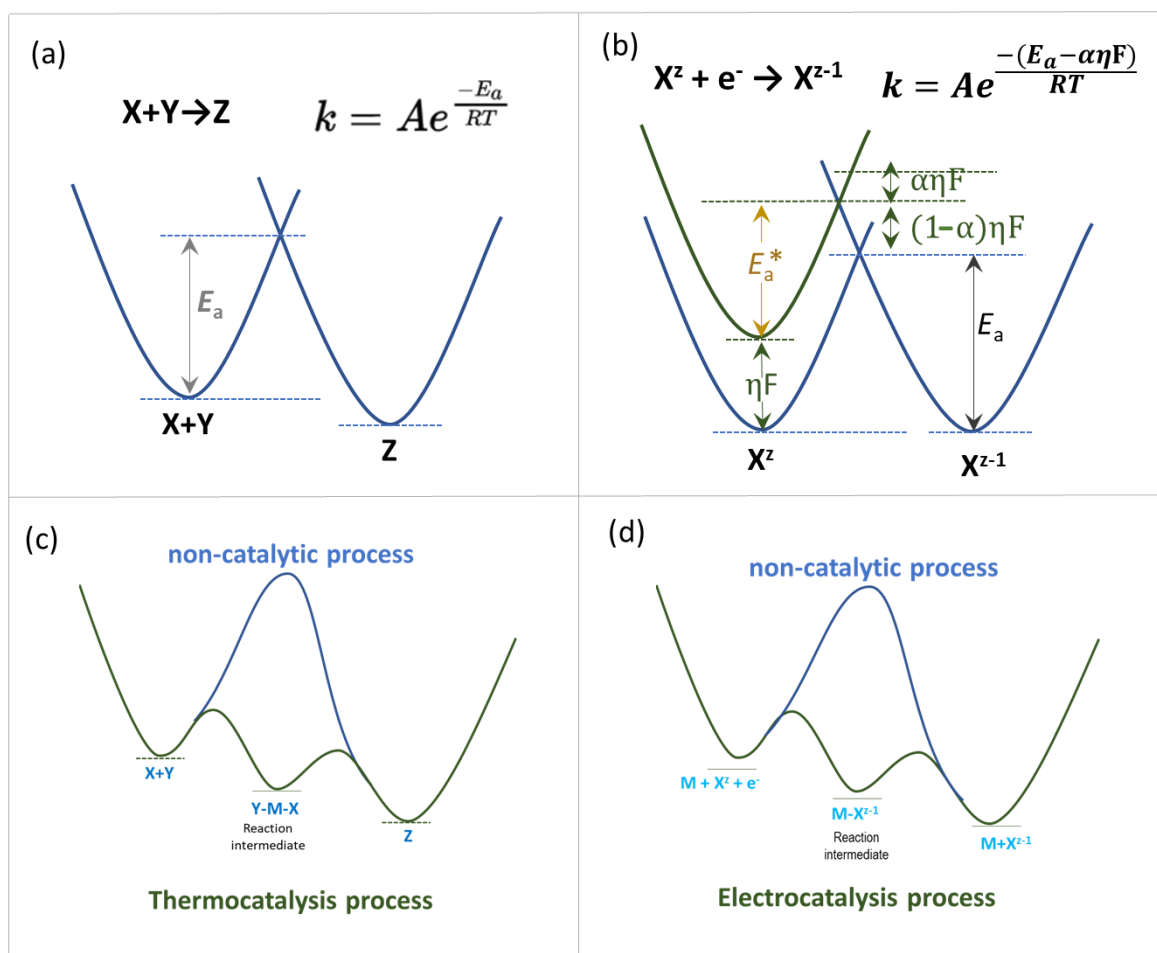


Figure 1. (a) conventional chemical reaction, (b) electrochemical reaction, (c) thermocatalysis process, and (d) electrocatalysis processes.

2.1 CO₂ reduction via thermocatalysis

In the thermocatalytic CO₂ hydrogenation/reduction process, temperature and pressure are the typical driving force to overcome the activation barrier and accelerate the reaction rate. Since nearly all the reactants are in contact with a thermocatalyst, the energy needed or released needs to be conducted through the reactants and thermocatalysts. The molar enthalpy change ($\Delta_r H^\ominus$) and Gibbs energy change ($\Delta_r G^\ominus$) of the typical CO₂ hydrogenation reactions are listed in Table 1. The conversion of some reactions in Table 1 is limited by the thermodynamic equilibrium, and a comprehensive thermodynamics analysis of these reaction can be found in Ref.⁵² From the viewpoint of carbon abatement, the H₂ used in CO₂ reduction must come from renewable sources such as solar powered water electrolysis other than carbon sources such as coal and natural gas. The thermocatalysts for CO₂ hydrogenation require simultaneous activation of CO₂ molecules and H₂ molecules, and many transition metals and metal oxides show good activity and selectivity.

Table 1. The molar enthalpy change ($\Delta_r H^\ominus$) and Gibbs energy change ($\Delta_r G^\ominus$) of typical CO₂ hydrogenation reactions (all components are in the gas state).

No.	Reaction equation	$\Delta_r H^\ominus$ kJ/mol	$\Delta_r G^\ominus$ kJ/mol
1	$\text{CO}_2 + \text{H}_2 \rightarrow \text{HCOOH}$	14.9	43.5
2	$\text{CO}_2 + \text{H}_2 \rightarrow \text{CO} + \text{H}_2\text{O}$	41.2	28.6
3	$\text{CO}_2 + 3\text{H}_2 \rightarrow \text{CH}_3\text{OH} + \text{H}_2\text{O}$	-49.3	3.5
4	$\text{CO}_2 + 4\text{H}_2 \rightarrow \text{CH}_4 + 2\text{H}_2\text{O}$	-165.0	-113.5
5	$\text{CO}_2 + 3\text{H}_2 \rightarrow 1/2\text{C}_2\text{H}_4 + 2\text{H}_2\text{O}$	-64.0	-28.7
6	$\text{CO}_2 + 3\text{H}_2 \rightarrow 1/3\text{C}_3\text{H}_6 + 2\text{H}_2\text{O}$	-83.6	-42.1
7	$\text{CO}_2 + 3\text{H}_2 \rightarrow 1/4\text{C}_4\text{H}_8 + 2\text{H}_2\text{O}$	-90.3	-45.2

8	$\text{CO}_2 + 3\text{H}_2 \rightarrow 1/2\text{C}_2\text{H}_5\text{OH} + 3/2\text{H}_2\text{O}$	-86.7	-32.4
9	$\text{CO}_2 + \text{H}_2 \rightarrow \text{C}_x\text{H}_y\text{O}_z \text{ (higher products)} + \text{H}_2\text{O}$	N.A.	N.A.

2.2 CO₂ reduction via electrocatalysis

In the electrochemical reaction, an overpotential (the potential difference between the thermodynamically determined equilibrium potential and the applied potential to make the reaction proceed) is applied to overcome the activation barrier. A good electrocatalyst can maximally reduce the overpotential required for driving a specific electrochemical reaction, thereby improving the utilization efficiency of electric energy. The electrocatalysis process can also be done by different catalytic mechanisms, as shown in Figure 2. In this review, we mainly discuss the case of the heterogeneous way in an electrocatalytic film (Figure 2c). Typically, a proton-electron couple is used as reactant to reduce CO₂ ($\text{CO}_2 + \text{nH}^+ + \text{ne}^-$) by electrocatalysis, among which the chemical potential of electrons can be adjusted by the applied electrode potential. This is different from the thermocatalysis process, where the chemical potential of H₂ is adjusted by pressure and temperature.

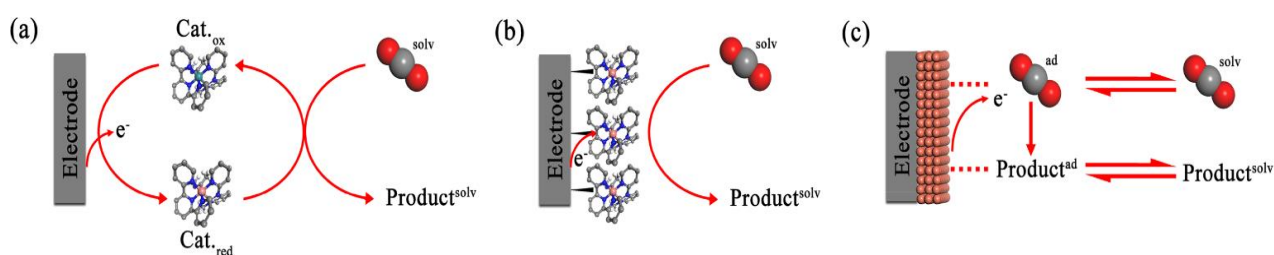


Figure 2. Schemes for CO₂ reduction by different catalytic mechanisms: (a) homogeneous, (b) immobilized, and (c) heterogeneous way in an electrocatalytic film. Reprinted with permission from ref.⁵³ Copyright American Chemical Society 2020.

Table 2 lists the basic information of the typical CO₂ electroreduction reaction. Since the electrochemical CO₂ reduction process involve the proton-electron couple and the equilibrium potentials of these reactions are close to 0 V vs. reversible hydrogen electrode (RHE), the hydrogen evolution reaction (HER) ($2\text{H}^+ + 2\text{e}^- \rightarrow \text{H}_2$, $E^0 = 0$ V vs. RHE) will compete with CO₂ reduction reactions. How to suppress HER is an essential topic in CO₂ electrochemical reduction. Figure 3 shows the schematic diagram of CO₂ reduction steps via electrochemical methods. Various intermediates and paths are proposed. In the electroreduction of CO₂, key reaction intermediates such as *CO, *OH, COOH*/CHO* and OCHO* would determine the final products.

Table 2. Basic information of CO₂ electrochemical reduction half-reactions.⁵⁴

No.	Reaction equation	Equilibrium potential E° (V vs. RHE)
1	$\text{CO}_2 + 2\text{H}^+ + 2\text{e}^- \rightarrow \text{HCOOH}$	-0.20 (for pH < 4); -0.20 + 0.059[pH-4] (for pH > 4)
2	$\text{CO}_2 + 2\text{H}^+ + 2\text{e}^- \rightarrow \text{CO} + \text{H}_2\text{O}$	-0.10
3	$\text{CO}_2 + 4\text{H}^+ + 4\text{e}^- \rightarrow \text{HCHO} + \text{H}_2\text{O}$	-0.07
4	$\text{CO}_2 + 6\text{H}^+ + 6\text{e}^- \rightarrow \text{CH}_3\text{OH} + \text{H}_2\text{O}$	0.02
5	$\text{CO}_2 + 8\text{H}^+ + 8\text{e}^- \rightarrow \text{CH}_4 + 2\text{H}_2\text{O}$	0.17
6	$2\text{CO}_2 + 12\text{H}^+ + 12\text{e}^- \rightarrow \text{C}_2\text{H}_4 + 4\text{H}_2\text{O}$	0.08
7	$2\text{CO}_2 + 12\text{H}^+ + 12\text{e}^- \rightarrow \text{C}_2\text{H}_5\text{OH} + 3\text{H}_2\text{O}$	0.09
8	$\text{CO}_2 + n\text{H}^+ + n\text{e}^- \rightarrow \text{C}_x\text{H}_y\text{O}_z \text{ (higher products)} + m\text{H}_2\text{O}$	NA

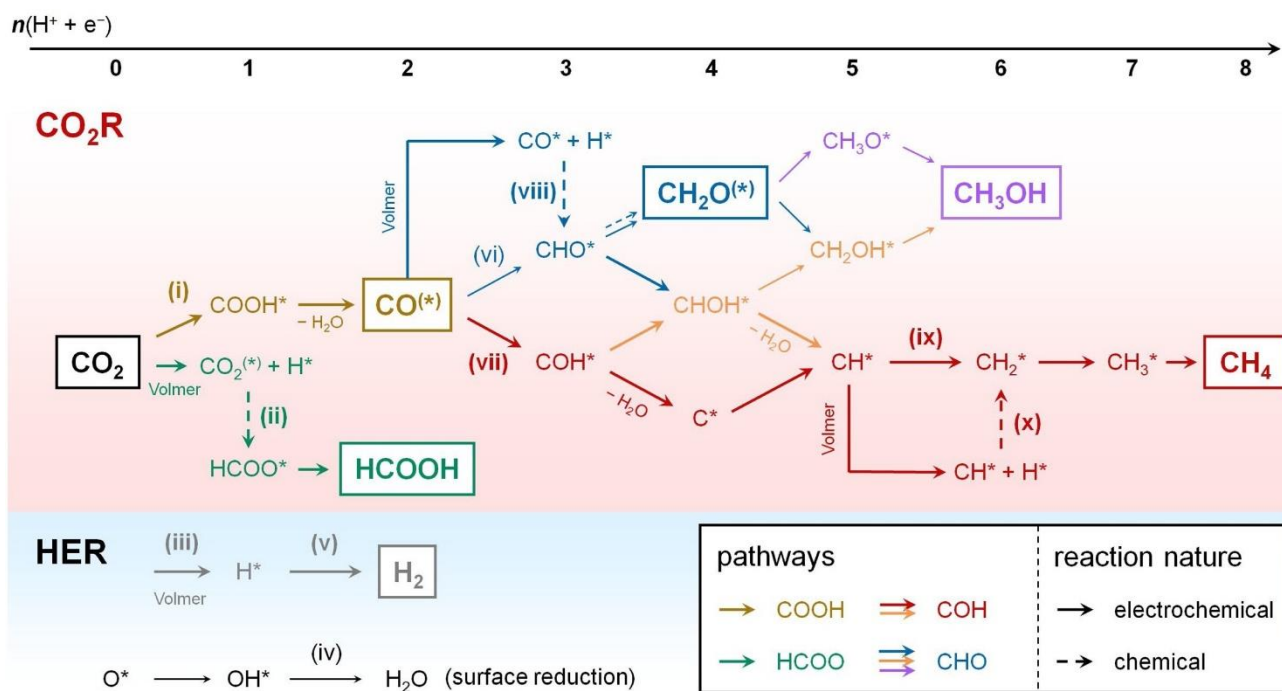


Figure 3. Schematic diagram of electrochemical CO₂ reduction reaction steps. Reprinted with permission from Ref.⁵⁵ Copyright Elsevier 2020.

Regarding the electrocatalysts for CO₂ reduction, Hori et al.⁵⁶ did a systematical investigation of CO₂ reduction on various metals, and they can be divided into four groups of materials according to the main products: (1) Pd, Ni, and Mo et al. as carbophilic metals primarily produce H₂ doing HER side reaction; (2) Au, Ag, and Zn as nonoxophilic and noncarbophilic metals primarily produce CO; (3) Pb, Sn, In, Bi, and Sn as oxophilic and noncarbophilic metals primarily produce formate; (4) Copper is unique for producing higher products beyond CO and formate.⁵⁷ (Figure 4a) The decorating metal on Cu in Figure 4b shows the relative binding strengths of CO* and OH* to those of Cu (Figure 4b) also determines the selectivity of electrochemical CO₂ reduction.

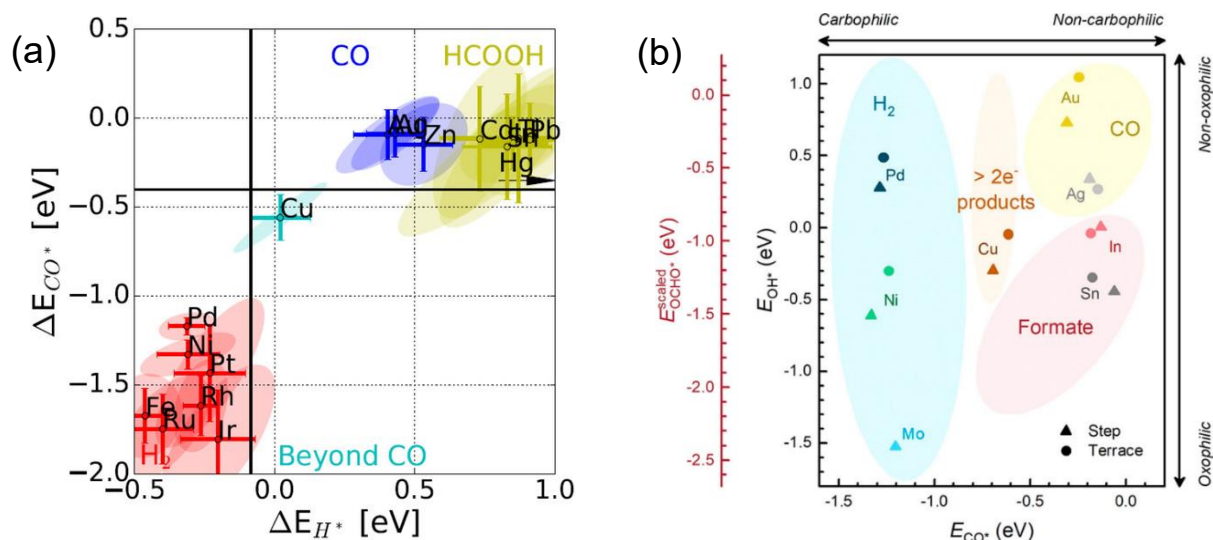


Figure 4. (a) Relationship between the binding energies of the intermediates *CO and *H of various metals with primary products in electrochemical CO_2 reduction. Reprinted with permission from Ref.⁵⁷ Copyright Wiley-VCH 2017. (b) Relationship between CO^* binding energy and OH^* binding energy with primary products in CO_2 reduction. Reprinted with permission from Ref.⁵⁸ Copyright American Chemical Society 2020.

3. Reduction of CO_2 to chemicals and fuels

In this section, the conversion of CO_2 to various chemicals and fuels via thermocatalysis and electrocatalysis will be summarized and compared according to their products. The typical thermodynamics, thermocatalysts and electrocatalysts, as well as reaction mechanisms, are summarized and discussed.

3.1 CO_2 to formic acid or formate

Formic acid is considered a promising hydrogen energy carrier.⁵⁹ Reduction of CO_2 by hydrogen to formic acid ($CO_2(g) + H_2(g) \leftrightarrow HCOOH(g)$, $\Delta G(298K) = 43.5$ kJ/mol, $\Delta H(298K) = 14.9$ kJ/mol) is a thermodynamically unfavorable reaction.⁵² The standard equilibrium constant of the reaction is only

2.4×10^{-8} at 298 K. Therefore, nearly all thermocatalytic CO₂ hydrogenation to formic acid is conducted by adding organic or inorganic bases to shift the reaction equilibrium to formate. To recover formic acid from formate, acidification or separation is required. Supported metal catalysts are the typical heterogeneous thermocatalysts used for this reaction, among which metal sites can activate hydrogen while the support can adsorb and activate CO₂.⁶⁰ For example, CeO₂ and ZnO supported palladium,⁶¹ heterogeneous gold metal,^{62, 63} and silica-tethered iridium,⁶⁴ are widely investigated for CO₂ hydrogenation to formate. Iridium⁶⁵ and ruthenium⁶⁶ molecular catalysts also demonstrated highly active for formate production. Theoretical calculation of CO₂ hydrogenation to formic acid on Ni(111) and Ni(110)^{67, 68} shows that CO₂ hydrogenation to formate intermediate is more favorable than to carboxyl intermediate, as shown in Figure 5. However, further hydrogenation of formate to formic acid by surface H is hindered by a larger activation energy barrier. In contrast, for the carboxyl-mediated route to HCOOH, the first H addition to CO₂ presents a barrier much larger than the second hydrogen addition. Additionally, *COOH can decompose to *CO and *OH. Understanding the mechanism of formic acid formation can provide an important reference for explaining the formation of higher-order products, so research in this area still needs to be strengthened.

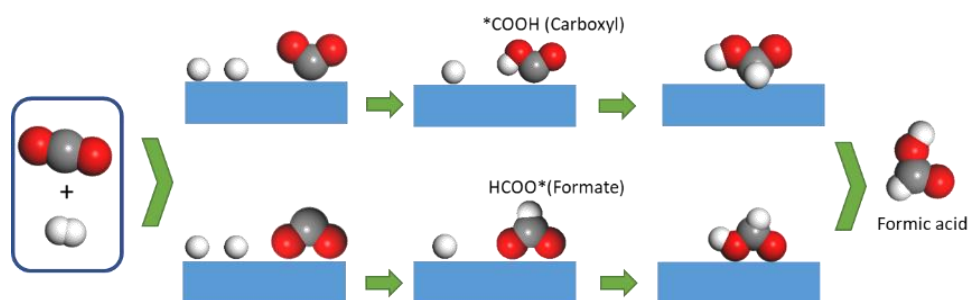


Figure 5. two pathways of thermocatalytic CO₂ hydrogenation to formic acid via *COOH (carboxyl) and HCOO*(formate) intermediates.

In contrast, the electroreduction of CO₂ to formic acid will not be limited by thermodynamics due to the introduction of external force (electricity). The equilibrium potential of this reaction is -0.20 V versus RHE for formic acid (pH < 4), or the equilibrium potential is $-0.20 + 0.059[\text{pH}-4]$ (for pH > 4). Various molecular catalysts were investigated for electrocatalytic CO₂ reduction to formic acid, including Rh, In and Sn metalloprotoporphyrins⁶⁹, Ir^{70, 71}, and Ru⁷² based molecular complex. In addition, tin⁷³, bismuth⁷⁴, indium⁷⁵, and lead⁷⁶ based metal electrocatalysts⁷⁷ are reported to be effective for formic acid / formate production. Recently, a Cu₂O nanoparticle film synthesized by square-wave electrochemical redox cycling of Cu foils afforded up to 98% Faradaic efficiency for electroreduction of CO₂ to nearly pure formate under ≥ 45 atm CO₂ in bicarbonate catholytes.⁷⁸ It should be noted that in most cases, the obtained formic acid is dissolved in the electrolyte, so all-solid-state reactors are designed to produce pure formic acid.^{79, 80}

In electrocatalysis CO₂ reaction, a CO₂⁻ anion bound to the catalyst surface is firstly generated by the first electron transfer to CO₂. This anion can be further reduced to formate through a following electron couple proton transfer step as shown in Figure 6. The former is similar to the formate-intermediate mechanism in the thermocatalysis process. CO₂ can also be electrochemically reduced via *COOH intermediate through an electron-coupled proton transfer step, which can be further separated into two elementary steps, i.e. the electron transfer and proton transfer steps. Further reduction of *COOH can obtain *CO or HCOOH. In addition, protons can also be firstly electro reduced on catalyst surface to a bonded hydrogen atoms, then CO₂ is adsorbed to form carboxyl or formate, which is quite similar with the process in the thermocatalysis process (Figure 5). The reaction pathways of CO₂ reduction will depend on catalyst⁵⁴. The thermodynamic theory of multiple proton-electron transfer predicts that for all reactions in which only 2 electrons (that is n = 2, such as producing formic acid or CO) are

transferred, ideal catalysts will exist that are able to catalyze the corresponding redox reactions in both directions, namely, both reduction and oxidation, with negligible overpotentials.⁸¹ Therefore, the process of electroreduction of CO₂ to formic acid is expected to achieve high electricity utilization on high performance catalysts.

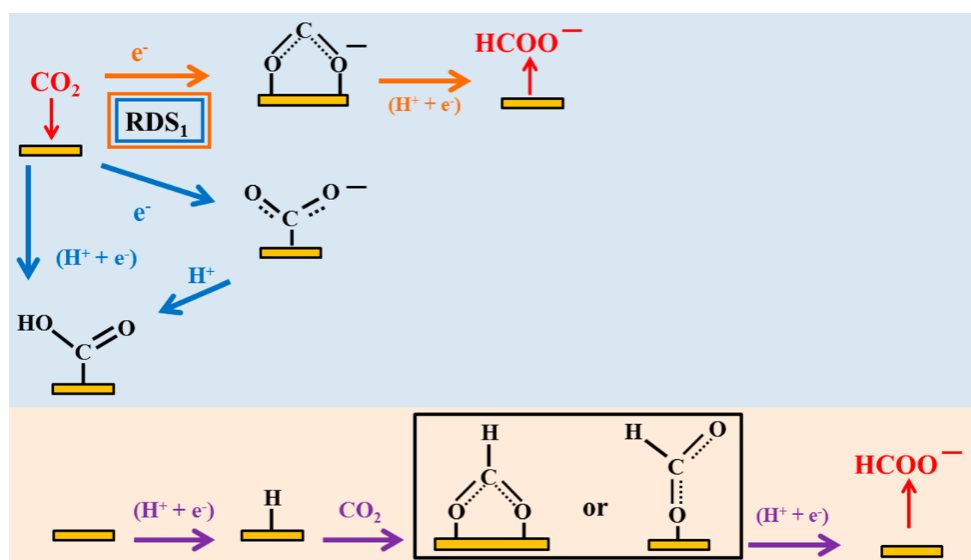


Figure 6. Reaction elementary steps of electrocatalytic CO₂ to formate (formic acid). Reprinted with permission from Ref. ⁵⁴ Copyright 2015 American Chemical Society.

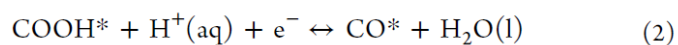
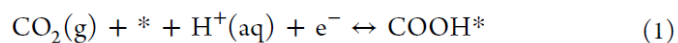
3.2 CO₂ to carbon monoxide

Reduction of CO₂ to carbon monoxide (CO) via thermocatalysis is also known as the reverse water-gas shift reaction ($\text{CO}_2 + \text{H}_2 \leftrightarrow \text{CO} + \text{H}_2\text{O}$, ΔG (298 K) = 28.6 kJ/mol, ΔH (298 K) = 41.2 kJ/mol).

This reaction is a thermodynamically less favorable, endothermic reaction. Pressure has little effect since the number of molecules does not change after the reaction. A CO₂ equilibrium conversion of only ~5% can be reached at 100 °C and of ~80% can be obtained at 800 °C with H₂/CO₂ molar ratio of 4.⁵² Oxides supported precious metals Pt⁸², Pd⁸³, Rh⁸⁴, and Au⁸⁵ and nonprecious metals Cu⁸⁶, Fe⁸⁷,⁸⁸, and Ni⁸⁹ were reported to be active and selective toward the production of CO. Typically, the

dispersion or particle size and surface morphology of metals will affect the activity and selectivity for CO.⁹⁰ In addition, the reaction temperature can also tune the selectivity of CO₂ hydrogenation to CO. For example, a Ni supported on CeO₂, which is highly selective for CH₄ (> 99 %) below 300 °C, can shift to 90% CO at 700 °C.⁵² The elementary reaction steps of CO production are suggested via carboxyl intermediate, as shown in Figure 5. Decomposition of carboxyl generates *CO and *OH, then CO desorbs while *OH is further reduced to H₂O. Another possible route is via a direct C-O bond cleavage pathway.⁹⁰

The electrochemical reduction of CO₂ to CO has an equilibrium potential of -0.10V versus RHE. It is a two-electron and two-protons transfer process. Thermodynamically, it can proceed via two proton-coupled electron transfer (PCET) process⁹¹ as follows:



Nørskov et al.⁹¹ calculated the trends in the electrocatalytic activity of metals and enzymes for CO₂ reduction to CO. Figure 7 shows the free energy diagrams for CO₂ electroreduction to CO on Au(211) and Pt(211) surface. For Au surface with weak adsorption, the first PCET step is the rate-determining step, while for Pt surface with strong adsorption, the reaction rate is limited by the desorption of CO. Experimental results show that gold and silver-based catalysts are highly selective for CO₂ electrochemical reduction to CO.^{92, 93} Kinetic studies of CO₂ reduction to CO on planar silver and gold electrodes in aqueous electrolytes are conducted by mathematical modeling method and the results show that gold is more selective for CO compared with silver⁹⁴. A recent study indicate that CO₂ electroreduction cannot occur on copper, gold and silver electrodes without metal cations in solution.⁹⁵

The partially dissolved metal cations are necessary to stabilize the CO_2^- intermediate via a short-range electrostatic interaction. In addition, earth-abundant metal (Ni, Fe, and Co) and nitrogen-doped carbon electrocatalysts also showed high selectivity for CO_2 reduction to CO ⁹⁶⁻⁹⁸. Pyrrolic nitrogen ligands selectively bind Ni atoms in a distorted square-planar geometry that strongly resembles the active sites of molecular metal–porphyrin catalysts is considered as the active sites for the reaction.⁹⁹ In addition, syngas (mixture of H_2 and CO) can be obtained on some catalysts with lower selectivity for CO , for example, palladium-based electrocatalysts¹⁰⁰. In CO_2 reduction to CO process, the side reaction (hydrogenation evolution reaction) will cause a pH increase near the electrode surface. Thus, CO_2 will be consumed and its surface concentration on electrocatalysts decrease, leading a lower Faraday efficiency and carbon efficiency.

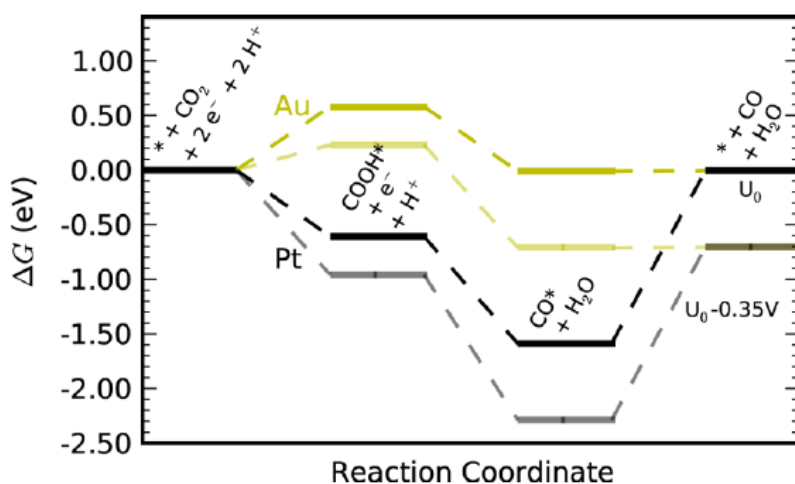


Figure 7. Free energy diagrams for CO_2 electroreduction to CO on Au(211) and Pt(211) at the reversible potential, U_0 , for CO evolution and at a 0.35 V overpotential. Reprinted with permission from ref⁹¹. Copyright 2013 American Chemical Society.

Recently, Jaramillo and co-workers¹⁰¹ investigated Ni, N-doped carbon catalyst which works both as

an electrocatalyst for the reduction of CO_2 to CO and a thermal catalyst for CO_2 to CO via the reverse water gas shift (RWGS) reaction as shown in Figure 8a. Advanced characterization techniques reveal that this catalyst facilitates RWGS on dispersed Ni sites in agreement with CO_2 electroreduction active site studies. A generalized reaction driving force that includes temperature and potential is constructed to facilitate faster kinetics in electrochemical CO_2 reduction relative to RWGS due to lower intrinsic barriers (Figure 8b and 8c).

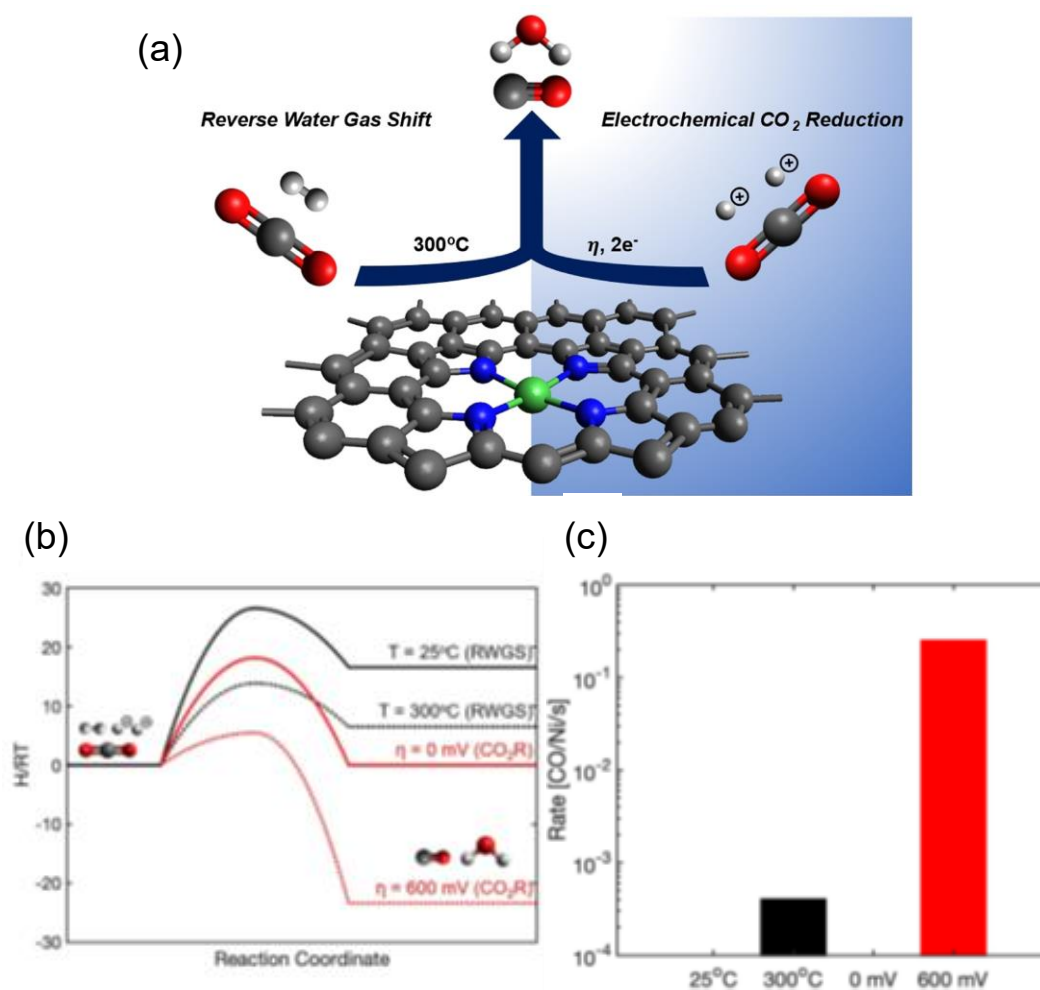


Figure 8. A Ni, N-doped carbon catalyst works both as an electrocatalyst and thermocatalyst for CO_2 reduction to CO. Reprinted with permission from ref^[10]. Copyright 2021 Wiley.

3.3 CO_2 to methanol

Methanol, an important platform molecule, is considered as a promising energy carrier or alternative fuel as well. Research progress on heterogeneous catalysts for methanol synthesis from carbon dioxide hydrogenation has been well reviewed.^{18, 102, 103} Various thermocatalysts including Pd/ZnO catalysts¹⁰⁴, In₂O₃ based catalysts^{105, 106}, ZnO-ZrO₂ solid solution catalyst¹⁰⁷, MZrO_x (M = Cd, Ga) solid-solution catalysts¹⁰⁸ for direct CO₂ hydrogenation to methanol have been investigated. The active sites for CO₂ hydrogenation to methanol on Cu/ZnO catalysts are intensively studied¹⁰⁹ but still in debate¹¹⁰. The binding energies of key intermediates for CO₂ hydrogenation to methanol over oxide-supported copper are the key to the selectivity⁸⁶. In addition, both Pd and oxygen vacancy are found to affect the performance of CO₂ hydrogenation to methanol over Pd/In₂O₃¹¹¹. A special Ni-Ga catalyst was discovered to be highly active and selective for carbon dioxide reduction to methanol.¹¹² Similar nickel–gallium catalysts were also investigated for catalyzing the electrochemical reduction of CO₂ but the main products are methane, ethylene, and ethane.¹¹³ In addition, copper-zinc alloy catalysts, which is selective for methanol in thermocatalyst, exhibited Faradaic efficiency values as high as 33.3% for C₂H₄ in CO₂ electroreduction.²⁹

In the electrocatalytic conversion of carbon dioxide to methanol on transition metal surfaces, Jaramillo et al.¹¹⁴ found that all metals studied (Au, Ag, Zn, Cu, Ni, Pt, and Fe) can produce methane or methanol, although the selectivity is very low. The metal surface's binding energy for CO is regarded as the key factor for their activity and selectivity towards methanol and methane. Other metals, such as molybdenum–bismuth bimetallic chalcogenide, is reported to be efficient for the electrocatalytic reduction of carbon dioxide to methanol.¹¹⁵ Different from metal catalysts, molecular catalysts such as iron tetradentate phosphine complex are found to be selective (Faraday efficiency of 68.5 %) for electrocatalytic reduction of CO₂ to methanol.¹¹⁶ Moreover, a molecular cobalt phthalocyanine catalyst

immobilized on carbon nanotubes catalyzes the six-electron reduction of CO₂ to methanol with appreciable activity and selectivity.¹¹⁷ In addition, the pyridinium ion is found to be a novel homogeneous catalyst for reducing CO₂ to methanol with faradaic yields of up to 30% at hydrogenated Pd electrodes.¹¹⁸ Although some progress has been made, metallomacrocyclic catalysts are still far from meeting the practical requirement for direct electrochemical CO₂-to-methanol conversion.¹¹⁹ Hernandez et al. compared the technical, environmental, and economic feasibility of CO₂ conversion to methanol via thermocatalytic and electrocatalytic technology¹²⁰. It is suggested that the CO₂ electroreduction process must be optimized (improving catalysts performance and mass transfer) to achieve industrial production rates and the same maturity level of the thermocatalytic approach.

3.4 CO₂ to methane

Methane (CH₄), as the main component of natural gas, is also a greenhouse gas. Methane is emitted during the production and transportation of fossil fuels and from livestock and other agricultural practices, land use, and by the decay of organic waste in municipal solid waste landfills. Hydrogenation of CO₂ to CH₄, also known as methanation, can make synthetic natural gas and replace part of natural gas by using the existing gas distribution system. If renewable hydrogen is considered, the carbon emission can be reduced. CO₂ methanation is a thermodynamically more favorable reaction compared with CO₂ reduction to CO. However, a catalyst facilitating high CO₂ conversion and selectivity to CH₄ needs to be developed due to kinetic limitations. Figure 9 lists the possible reaction mechanism for CO₂ methanation. Ni-based catalysts are mostly studied for CO₂ methanation because of their high activity and low cost. However, conventional alumina-supported Ni catalysts are easily deactivated because of coke deposition and the sintering of Ni particles during the strongly exothermic process.

Therefore, other materials, such as hydrotalcite-derived materials and bimetallic catalysts (such as Ni-Fe) for CO₂ methanation, are investigated.¹²¹ Other noble metals such as rhodium, ruthenium, and palladium dispersed on various supports were also investigated for CO₂ methanation, but Ni-based ones are still the most promising for industrial applications considering its activity and cost¹⁵. Thermodynamically, a lower temperature is more beneficial for higher CH₄ selectivity and equilibrium conversion of CO₂. Thus, efforts are also made to conduct CO₂ methanation at low temperatures, which can also reduce the sintering of catalysts.¹²² Three possible reaction mechanisms of CO₂ methanation on Ni(111) surface were proposed¹²³. The first one is via formate intermediate, while the second is the direct dissociation of *CO₂ to *CO and *O. The last mechanism contains a reaction intermediate of C(OH)₂*. Among these three paths, the direct dissociation is suggested as the optimal path. A recent mechanistic study of CO₂ methanation over Rh/TiO₂ catalysts¹²⁴ shows that the methane production rate per surface Rh atoms increases as metal particle size increases up to ca. 7 nm. Smaller Rh particles tend to bind *CO intermediate stronger than larger ones, and *CO dissociation is aided by the presence of H species and that a likely surface intermediate is Rh carbonyl hydrides. Apart from the active nickel sites, the support also plays an essential role in CO₂ methanation.¹²³ The support can affect CO₂ adsorption, CO₂ activation, methanation mechanism, and deactivation process.⁹⁰

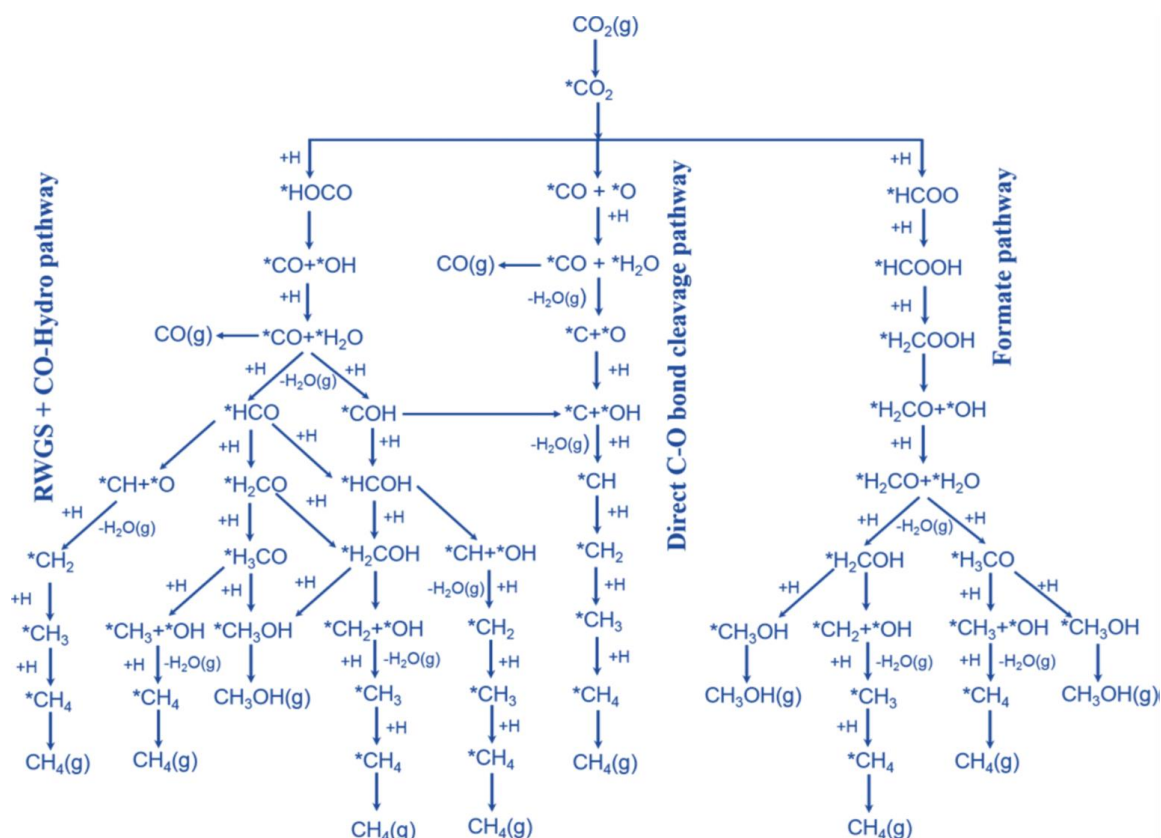


Figure 9. Possible reaction pathways of CO₂ hydrogenation to CO, CH₃OH, and CH₄. *(X) indicates adsorbed species. Reprinted with permission from Ref.⁹⁰ Copyright 2015 American Chemical Society.

In the electrocatalytic conversion of carbon dioxide to methane, eight electrons and eight protons need to be transferred. The selectivity to methane (Faraday efficiency) via CO₂ electroreduction is generally low compared with formate and CO, but CH₄ as a product has been observed on various transition metal surfaces, including Au, Ag, Zn, Cu, Ni, Pt, and Fe.¹¹⁴ The activity descriptors for CO₂ electroreduction to methane on transition-metal catalysts were theoretically analyzed by Norskov and co-workers¹²⁵, as shown in Figure 10. For weak adsorption metal surfaces such as Au and Ag, the reaction is limited by the protonation of CO₂ to COOH. For other metals such as Cu, Ni, Pt, Rh, and Pd, it is found that the protonation of adsorbed CO is singled out as the most important step dictating the overpotential. Cu is predicted to be the best of all the seven metals investigated, but a larger

overpotential is needed to overcome the kinetics barrier. In the multi-electron transfer reduction of CO_2 , a similar universal energetic scaling between *CO and *HCO intermediates leads to an overpotential for the eight-electron reduction of CO_2 to methane.¹²⁵ The binding energy *CHO must be strengthened relatively to *CO to make the catalyst more effective as reducing CO_2 to CH_4 .

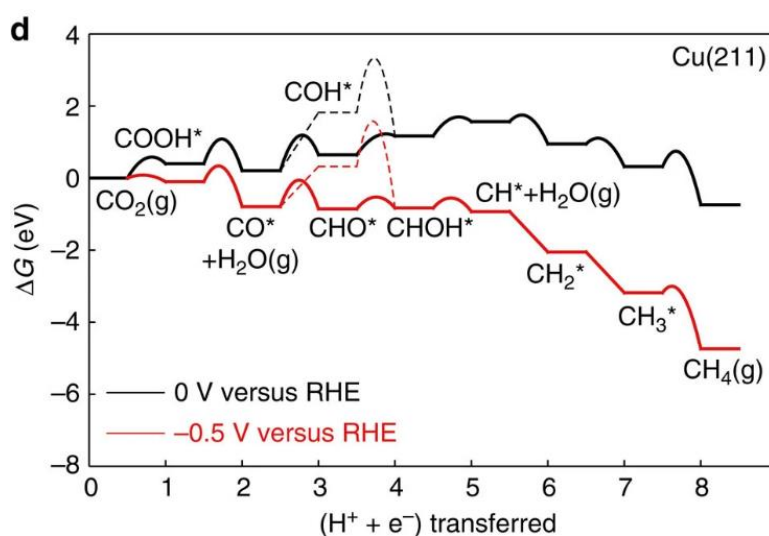


Figure 10. (d) free energy diagram for the reduction of CO_2 to CH_4 on Cu(211) at 0 V and -0.5 V versus RHE.¹²⁶ Copyright the authors by Creative Commons Attribution 4.0 International License.

3.5 CO_2 to ethylene

Ethylene is widely used in the chemical industry, and it is one of the most globally produced organic compounds. Although the hydrogenation of CO_2 to ethylene is a thermodynamically favorable reaction, there are rare reports about the thermocatalytic hydrogenation of CO_2 to ethylene with high selectivity. With methanol as an intermediate, it is reported that CO_2 can be hydrogenated to ethylene and propene via bifunctional catalysts.²⁰ However, a significant amount of CO as a byproduct is observed. Controllable C-C coupling to selectively forming ethylene is quite challenging in thermocatalysis approach.

In contrast, CO₂ can be reduced to ethylene at high selectivity on copper based electrocatalysts in the electroreduction process. Various methods, including tuning surface oxygen²⁸, fluorine modification³⁰, surface modification¹²⁷, as well as structural control²⁷ of Cu catalysts and laser-prepared CuZn alloy catalyst²⁹, are used to enhance the selectivity to ethylene. In the electrocatalysis route, CO dimer is considered as the primary intermediate during the reaction process.¹²⁸ It is also found that C₂ products are favored in CO₂ electrochemical reduction under alkaline conditions. The mechanistic insights of a recent work¹²⁹ elucidate how reaction conditions can stabilize critical intermediates and lead to significant enhancements in selectivity and activity towards higher value added C₂ products.

3.6 CO₂ to ethanol

Ethanol is another important industrial chemical and alternative fuel. Various catalysts, such as Cu@Na-Beta catalysts¹³⁰, ordered Pd–Cu Nanoparticles¹³¹, supported Co₂C¹³² or Co¹³³ catalysts, and promoted Rh/SiO₂ catalysts¹³⁴ are reported to be highly active and selective for thermocatalytic CO₂ hydrogenation to ethanol. However, the ethanol yield is far below methanol under similar reaction condition, further suggesting the selective C–C coupling is quite challenge in thermocatalysis.

In the electrocatalysis process, copper-based electrocatalysts dominated in the CO₂ electroreduction to ethanol process. The oxygen content controlled by selective oxidation/reduction in bimetallic AgCu foam electrocatalysts plays an important role in ethanol formation from CO₂.¹³⁵ Oxide-derived Cu_xZn catalysts were reported to selectivity reduction of CO₂ to ethanol via electrocatalysis way.¹³⁶ It is demonstrated that the selectivity of CO₂ reduction toward ethanol could be tuned by introducing a cocatalyst (Zn sites) to generate an in-situ source of mobile CO reactant, which can promote the ethanol production over ethylene.¹³⁶ In the electrocatalytic process, the atomically dispersed copper can even

form metallic clusters and act as active sites for selective electrocatalytic CO₂ reduction to ethanol¹³¹. Abild-Pedersen et al.¹³⁷ suggested that the carbon and hydroxide binding strengths will determine the trends in C₂ oxygenate/hydrocarbon selectivity during CO₂ electrochemical reduction process. In short, the selectivity of ethanol in both thermocatalysis and electrocatalysis processes remains low, and more effective catalysts are needed. Understanding the oxygenate/hydrocarbon formation mechanism will facilitate the design of more efficient catalysts.

3.7 CO₂ to other higher carbon (C₂+) products

In the electrocatalysis approach, copper catalysts show the highest potential for producing higher carbon products. A total of 16 different CO₂ reduction products were observed on copper.¹³⁸ A scheme forming multi-carbon products is proposed, as shown in Figure 11. Enol-like surface intermediates are proposed to account for the observed eleven distinct C₂⁺ oxygenated products including aldehydes, ketones, alcohols, and carboxylic acids. Recently, electrochemical reduction of carbon dioxide to 1-butanol on oxide-derived copper, although the Faradaic efficiency is only 0.056 %, with a 1-butanol partial current density of $-0.080 \text{ mA cm}^{-2}$ at -0.48 V vs. RHE).¹³⁹ In contrast, Cu typically produces only single carbon atom products (e.g., CO, CH₄, and methanol) in gas-phase thermocatalysis. Theoretical study of C-C coupling in CO₂ electroreduction on copper electrodes¹⁴⁰ suggests that the control of hydrogen (proton and electron pairs) chemical potential by the applied potential at room temperature is unique to the electrochemical environment. In addition to Cu, some other catalysts show obvious selectivity to produce higher carbon products. For example, the electrocatalytic reduction of CO₂ to acetic acid can be achieved by a molecular manganese corrole complex immobilized on a carbon paper electrode¹⁴¹ with a faradaic efficiency of 63 % and a turnover frequency of 8.25 h^{-1} .

Long-chain hydrocarbons by CO₂ electroreduction using polarized nickel catalysts are also achieved although the Faradaic efficiencies is only up to 6.5% .³² How to improve the selectivity of advanced carbon products will be an important research direction for electrochemical CO₂ reduction in the future.

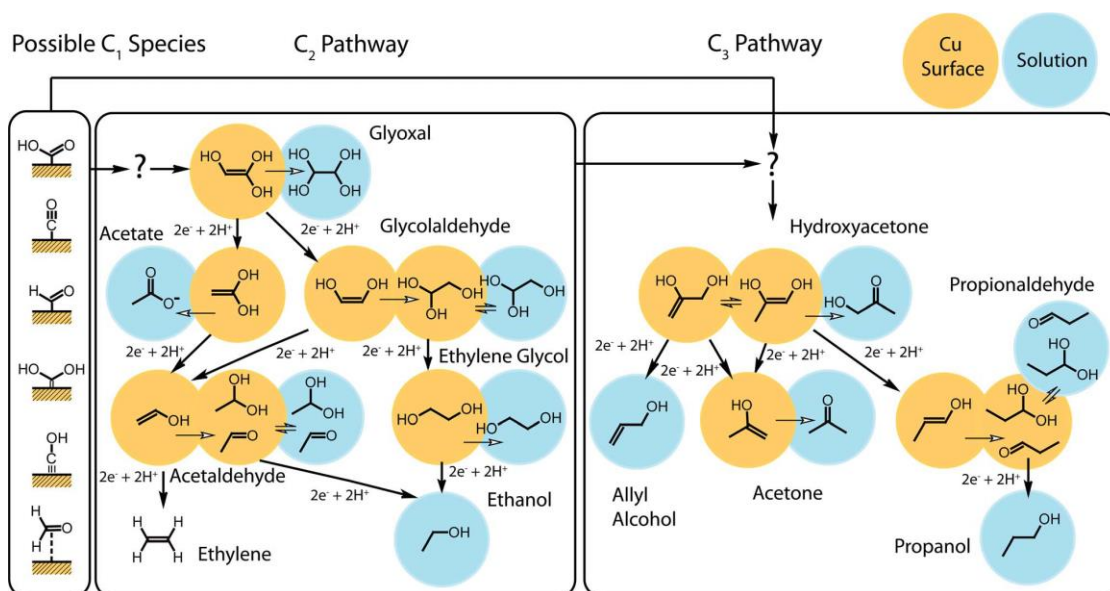


Figure 11. Proposed reaction pathway for C₂ and C₃ products with enol-like surface intermediates on Cu surface. Adopted with permission from Ref ¹³⁸, Copyright 2012 The Royal Society of Chemistry.

Regarding the progress of CO₂ reduction to higher carbon products, the thermocatalysis approach made progress far beyond electrocatalytic processes. In the thermocatalytic CO₂ hydrogenation approach, complex products such as light olefins²⁰, aromatics^{22, 142}, gasoline¹⁴³, and liquid fuels^{144, 145} with decent yield have been reported. Typically, in these process, bifunctional catalysts are used with the first catalyst to generate methanol from CO₂ hydrogenation, then convert methanol to high-value products on another catalyst. In contrast, Fischer–Tropsch synthesis (FTS)-based CO₂ hydrogenation is another different process, which combines the reduction of CO₂ to CO via the reverse water gas shift

reaction and hydrogenation of CO to hydrocarbons via FTS. These FTS based CO₂ hydrogenation processes can produce lighter olefins¹⁴⁶, C₅+ products such as gasoline and diesel liquid fuels and other value-added chemicals such as aromatics and isoparaffins¹⁴⁷. For instance, Fe- and FeCo-based catalysts can achieve $\geq 54.6\%$ CO₂ conversion and $\geq 47.0\%$ C₅+ selectivity. CO₂ FTS can also produce higher alcohols (C₂+OH)^{148, 149}. In both thermocatalytic and electrocatalytic CO₂ conversion process, the surface science of the catalyst regulates C–C coupling process.¹⁵⁰ Understanding surface science under reaction conditions will play an important role in the design and development of catalysts.

4. Thermocatalysis and electrocatalysis coupled system

There are usually two ways to combine the advantages of thermocatalysis and electrocatalysis. One is to conduct the electrocatalytic CO₂ reduction at high temperature and pressure¹⁵¹⁻¹⁵³ (to introduce thermocatalysis), the other is to apply the electric field in the thermocatalytic CO₂ reduction process¹⁵⁴⁻¹⁵⁷. Both methods have been studied, and some progress has been made. For example, compared with the CO₂ electrochemical reduction at room temperature, electrolysis of CO₂ ($2\text{CO}_2 \rightarrow 2\text{CO} + \text{O}_2$) at high temperatures (600 -1000 °C) exhibits higher current density and energy efficiency.¹⁵¹ In the high-temperature solid oxide electrolysis cells (SOECs), CO₂ and H₂O are fed in the cathode and typically reduced to CO (and H₂). Meanwhile, the O²⁻ ions are transferred to the anode and oxidized to O₂ through an O²⁻ ions membrane / conducting electrolyte. Ni and perovskite are the typical cathode materials. However, the cell degradation is the major challenge for the practical application of SOECs. The main degradation reasons for electrodes are agglomeration, depletion, carbon formation, poisoning, and decomposition. To address these problems, low temperature SOFC as a self-promoted reactor for CO₂ catalytic hydrogenation was proposed.¹⁵⁸

Coupled thermal–electrochemical catalysis could offer an attractive approach to upgrading CO₂ into value-added products if selective electrocatalysts and integrated devices were developed. There are some signs of progress have been reported. For example, CO₂ electrolyzer that operates at low overpotential and ambient pressure can selectively produce either CO or CH₄ with high selectivity (>95%) using Ir–ceria-based catalysts in an intermediate temperature (400 °C).¹⁵⁹ Moreover, coupling electrocatalytic CO₂ reduction with thermocatalysis enables the formation of a lactone monomer¹⁶⁰, which is not a typical product in single electrocatalytic or thermocatalytic processes. At last, in the catalyst development aspect, carbon-based materials¹⁰¹ and core–shell structured catalysts¹⁶¹ are proposed to bridge thermocatalysis and electrocatalysis and even photocatalytic process.

5. Conclusion and Outlook

Reducing CO₂ to valuable chemicals and fuels such as formic acid, carbon monoxide, methanol, methane, ethylene, ethanol, etc. by renewable hydrogen via thermocatalysis or by renewable electricity via electrocatalysis provides an attractive and sustainable way to addressing the climate change challenge. The thermocatalytic pathway can easily scale up and realize industrial-scale applications, but some of the reactions are limited by slow kinetic or thermodynamic equilibrium. In contrast, the electrocatalytic approach for CO₂ reduction is much less mature but has some advantages, such as low temperature and low pressure, using water as a hydrogen source, and is not restricted by thermodynamic equilibrium. In general, the thermocatalytic approaches have made more significant progress than electrocatalytic approaches in generating multi-carbon products via CO₂ reduction. Future research directions for CO₂ conversion process may consider the following two aspects.

(1) Electrochemical promoted thermocatalysis route

There is still much room for research to introduce an external field, such as an applying electronic field to facilitate the CO₂ reduction reaction.¹⁰ In addition, the synergies between electrocatalytic and thermocatalytic routes for CO₂ conversion to alcohols over Cu/ZnO catalysts has already proposed.¹⁶² Solid electrolyte CO₂ reduction cell operates at a relative high temperature (200-250 °C) can be considered. In that kind of reactor, CO₂ can be directly reduced by proton and electron on the electrocatalyst surface via electrocatalytic way ($x\text{CO}_2 + n\text{H}^+ + n\text{e}^- \rightarrow \text{product} + y\text{H}_2\text{O}$). Meanwhile, part of proton and electron will recombine to H₂ molecule or hydrogen atom on the catalyst surface and react with CO₂ via the thermocatalytic way ($\text{CO}_2 + \text{H}_2 \rightarrow \text{product} + \text{H}_2\text{O}$). It is worth to emphasize that, in traditional thermocatalytic reactor, the chemical potential of H₂ and CO₂ gas can only be adjusted by temperature and pressure. Here, the total chemical potential of hydrogen species and CO₂ can be further tuned by electric potential (for $\text{H}^+ + \text{e}^-$ part). At the same time, the electrical potential may affect or influence the electronic structure of the catalysts, which again promote the thermocatalytic process. To achieve this concept, development of high temperature (e.g. 200-250 °C) proton transfer membrane is necessary. Recent research shows that phosphoric acid-doped intrinsically ultramicroporous membranes can operate at 200 °C for fuel cells¹⁶³, which is very promising for this application.

(2) Tandem system / catalysts for CO₂ reduction

The tandem system includes electrocatalytic–thermocatalytic reaction scheme for CO₂ reduction to higher carbon products. For example, CO₂ can be reduced to syngas (CO and H₂, H₂ is generated via side reaction) via electrocatalytic approach and then the syngas can be converted to higher products such as C₃ oxygenates via thermocatalytic approach¹⁶⁴. The tandem system can also be a thermocatalytic process followed by electrocatalytic process, however, no such process has been

demonstrated and intensive research is necessary. The tandem thermocatalysts like the methanol synthesis via CO₂ hydrogenation catalysts as an intermediate, then the methanol can be further converted to higher products. Similar concept is applied in thermocatalytic process, for example, Jaramillo and coworkers developed a tandem gold-on-copper electrocatalyst which offers gold for CO generation and copper for further CO reduction to alcohols.¹⁶⁵ The rational design of bifunctional catalysts based on surface science and theoretical calculations has great potential to make breakthrough in both CO₂ thermocatalytic and electrocatalytic. The recent rise of machine learning and artificial intelligence promises to speed up the development process.

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Author contributions

J. Gao drafted manuscript; Y. Liu revised the manuscript.

Competing interests

The authors declare no competing financial interests.

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