

1 Axial Coordination Tuning Fe Single-atom Catalysts for
2 Boosting H₂O₂ Activation

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4 Haoyang Fu ^{a,b#}, Jiaqi Wei ^{b#}, Guoliang Chen ^b, Minkai Xu ^a, Jiyuan Liu ^b, Jianghong Zhang ^b,
5 Ke Li ^c, Qianyu Xu ^a, Yunjie Zou ^a, Weixian Zhang ^a, Shibo Xi ^d, Xiaodong Chen ^b, Shuzhou Li
6 ^{b*}, Lan Ling ^{a*}

7
8 [#] *These authors contributed equally to this work.*

9
10 ^a State Key Laboratory for Pollution Control and Resource Reuse, College of Environmental
11 Science and Engineering, Tongji University, Shanghai 200092, China

12 ^b School of Materials Science and Engineering, Nanyang Technological University, 50
13 Nanyang Avenue, Singapore, 639798, Singapore

14 ^c Institute of Materials Research and Engineering, Agency for Science, Technology and
15 Research, 138634, Singapore

16 ^d Institute of Chemical and Engineering Sciences, Agency for Science, Technology and
17 Research, 1 Pesek Road, Jurong Island, Singapore 627833, Singapore

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21 coordination, Wastewater treatment

22 **Abstract**

23 Precisely regulating the coordination microenvironment of single-atom catalysts (SACs)
24 to achieve enhanced reactivity is significant and desired but still in its infancy. Herein, a
25 coordination-tuned and pyrolysis-free strategy is reported for the fabrication of a Fenton-like
26 SAC containing the axial five-coordinated configuration (Fe–N₅). The N species on the N-
27 doped graphene act as anchoring points for iron phthalocyanine (a typical Fe–N₄ complex) to
28 obtain isolated Fe–N₅ sites, which significantly modulates the electronic state of Fe atoms and
29 lowers the H₂O₂ activation barrier for •OH production. Moreover, the enriched pyridinic N
30 serve as contaminant adsorption sites shortening •OH diffusion distance, establishing a dual-
31 site reaction mechanism with Fe–N₅ sites. As such, the Fe–N₅ catalyst exhibits exceptional
32 Fenton activity towards catalytic oxidation of phenol ($k = 0.180 \text{ min}^{-1}$). Our work unravels the
33 dependence of Fenton activity on the single-atom coordination environment and provides a
34 platform for precise engineering of SACs.

35 **1. Introduction**

36 Advanced oxidation processes (AOPs) are considered as promising approaches to obtain
37 reactive oxygen species (ROS), which serve as strong oxidants in wastewater treatment [1], soil
38 remediation [2], cancer therapy [3,4], etc. The Fenton process is one of the most efficient AOPs
39 that can generate highly active hydroxyl radicals (•OH) from the reaction of Fe²⁺ and hydrogen
40 peroxide (H₂O₂) under ambient conditions [5]. However, a narrow pH range (3–4) for such
41 homogeneous reaction as well as accumulation of ferric hydroxide sludge at high pH
42 environments limit its large-scale applications, especially for cleaning up recalcitrant organic
43 contaminants in solution [6]. Heterogeneous Fenton-like catalysts in different types, including
44 Fe-containing minerals [7], Fe nanoparticles [8], and other Fe supported catalysts [9,10], can
45 extend the working pH range from acidic to alkaline, and be recovered without ferric hydroxide

46 precipitation. Nevertheless, the efficient utilization of Fe atoms in heterogeneous Fenton-like
47 catalysts remains a pivotal challenge ahead of their practical applications.

48 The discovery of Fe single-atom catalysts (SACs) bridges the gap between heterogeneous
49 and homogeneous Fenton catalysis. Atomically dispersed Fe single-sites in SACs are often
50 under the coordination of N/C atoms on a carrier, which exposes the active center almost
51 completely to reactants and intermediates, thus obtaining near 100% utilization of Fe atoms to
52 activate H₂O₂ for organic pollutants degradation [11-16]. The coordination configuration of Fe
53 single-atom sites has been demonstrated to play a decisive role in determining the catalytic
54 properties by modifying the scaffold such as changing the coordination number of Fe atoms,
55 doping with heteroatoms (N, P, S, etc.), and tuning the compressive strain [17-20]. Fe
56 macrocycles, such as Fe porphyrins and phthalocyanines, are the precursors most widely used
57 to prepare the Fenton-like catalysts [21, 22]. To date, however, limited progress has been made
58 in improving their Fenton activity and durability. In particular, the obtained catalysts have been
59 demonstrated a long-time degradation in performance due to the demetalation of Fe
60 macrocycles in solution [23, 24]. Although the high-temperature pyrolysis strategy was applied
61 to modify the geometric and electronic structure of metal macrocycles to overcome existing
62 drawbacks of catalysts, the serious destruction of the precursor by this strategy results in nearly
63 uncontrollable and complex coordination environments for single-atom metals, making it tough
64 to unravel the relationship between local architecture and catalytic activity [25-27]. As such,
65 achieving a rational structural design and geometric engineering of catalytic single-atom sites
66 to control their catalysis performances, as well as exploring the correlation between the catalyst
67 structure and the reactivity, is highly desirable, yet challenging till now.

68 Herein, we report a moderate and facile axial coordination strategy to obtain effective
69 Fenton-like catalyst with precisely designed isolated Fe–N₅ catalytic sites. The strategy utilizes
70 N-doped graphene (NG) with N atoms as the anchoring site for iron phthalocyanine molecules
71 ((C₈H₄N₂)₄Fe, FePc), resulting in well-preserved structure of Fe–N₅ sites on NG and therefore

72 successful modulation of the axial coordination of Fe single-atoms. The Fe–N₅ sites dispersed
73 N-doped graphene (FeN₅/NG) exhibits superior Fenton-like degradation of phenol (a typical
74 organic contaminant), a degradation rate constant of 0.180 min⁻¹, which exceeded most of the
75 state-of-the-art Fenton-like catalysts. Our approach combining experiments and numerical
76 simulations demonstrate the role of the pyridinic N site on NG is to adsorb phenol molecules,
77 with the Fe–N₅ site catalyzing •OH formation. Moreover, quantum calculations reveal that the
78 Fe–N₅ site provides less charge to 2OH* intermediate but more charge to OH* intermediate
79 compared to the Fe–N₄ site, giving rise to a lower energy barrier for •OH generation to improve
80 the catalytic performance. This work presents a paradigm for axial coordination tuning of SACs
81 and establishes both theoretical and experimental foundations of accurate structure–activity
82 relationships for the construction of efficient Fenton catalysis.

83 **2. Materials and Methods**

84 **2.1 Synthesis of FeN₅/NG catalyst**

85 The fabrication of FeN₅/NG was started with the modification of graphene oxide (GO).
86 Briefly, 1.5 mL of ammonia (28 wt%) and 100 μL of hydrazine hydrate (80 wt%) were mixed
87 with 400 mL of GO aqueous dispersion (0.4 g/L) into a 1 L three-neck flask. The resulting
88 mixture was put in an oil bath and heated at 95 °C for 60 min to form the reduced graphene
89 oxide (rGO). The as-synthesized rGO was then annealed at 600 °C for 240 min in a quartz tube
90 furnace under a 15 vol% Ar/NH₃ gas mixture. The NG was finally obtained after cooling to
91 25 °C. The FeN₅/NG catalyst was synthesized by admixing 100 mg of NG and 40 mg of FePc
92 in 10 mL of anaerobic deionized water, with magnetic stirring for 10 min, followed by freeze-
93 drying for 60 min. The FeN₅/NG catalyst was washed with water and ethanol several times to
94 remove uncoordinated FePc before use. For comparative studies, the Fe–N₄ sites dispersed on
95 the reduced graphene oxide (FeN₄/G) and Fe–N₄ sites dispersed on the NG (FeN₄/NG) were
96 also synthesized in the similar way, except that the modification of reduced graphene oxide in
97 FeN₄/G was under the Ar environment and the heating temperature was set to 600 °C during

98 anchor of Fe single atoms for FeN₄/NG. Moreover, a series of catalysts with different content
99 of pyridinic N species were prepared by adding a pyrolysis process (modulation of the pyrolysis
100 temperature from 500 to 900 °C) between the synthesis of NG and the single-atom anchoring
101 process for the investigation of correlation between phenol adsorption efficiency and pyridinic
102 N content. Increasing the pyrolysis temperature from 500 to 900 °C enables a significant change
103 in the N distribution of the catalyst without obvious loss of N content (Table S1). Samples
104 obtained after pyrolyzing at 500, 700, and 900 °C were denoted as FeN₅/NG-500, FeN₅/NG-
105 700, and FeN₅/NG-900, respectively, and some physicochemical properties of FeN₅/NG-500,
106 FeN₅/NG-700, and FeN₅/NG-900 are provided in Table S2.

107 **2.2 Analysis and characterization**

108 The powder X-ray powder diffraction (PXRD) spectra were obtained on a powder X-ray
109 diffractometer (Bruker D8 Advance; Bruker AXS, German) with a high-power Cu K α (40 kV,
110 40 mA, λ = 1.54178 Å) radiation source. Scanning/transmission electron microscopy (S/TEM)
111 was measured using Cs-corrected FEI TitanTM G² 60–300 instrument (FEI Ltd., Hillsboro,
112 USA) operating at 300 kV with energy dispersive X-ray spectroscopy (EDS) for analysis of
113 catalyst composition. X-ray photoelectron spectroscopy (XPS) analyses of samples were
114 conducted using ESCALAB 250Xi (Thermo Fisher Scientific, USA) with a monochromatic K-
115 Alpha source (1486.6 eV). An inductively coupled plasma atomic emission spectroscopy (ICP-
116 OES, Optima2000, PerkinElmer, USA) was used to measure the elemental compositions. The
117 X-ray absorption structure (XAS) was performed at the X-ray Absorption Fine Structure for
118 Catalysis (XAFCA) beamline of Singapore Synchrotron Light Source (SSLS) center with
119 stored electron energy of 2.2 GeV using transmission mode [28].

120 **2.3. Computation methods**

121 All spin-polarized calculations involving density functional theory (DFT) in the present
122 work are calculated by the Vienna Ab initio Simulation Package (VASP) program [29]. The
123 ion-electron interaction is described by the Projector augmented wave (PAW) pseudopotential

124 method [30]. The plane-wave basis set is cut off at 600 eV and 450 eV for lattice optimization
125 and geometry optimization of adsorption intermediate, respectively. Generalized gradient
126 approximation (GGA) with the revised Perdew-Burke-Ernzerhof (PBE) functional was applied
127 to determine the exchange-correlation energy [31]. The energy and force convergence
128 thresholds at which all atoms are released during the structure optimization iteration are set to
129 be 10^{-4} eV and 0.03 eV/Å. FeN₄C₂₀ porphyrin structures terminated by hydrogen atoms were
130 adopted to construct the FeN₄ model. The NC carrier was simulated by constructing three
131 carbon atoms substituted with nitrogen atoms on a periodic 10×10×1 graphene plane, and the
132 FeN₅ model is constructed by linking the FeN₄C₂₀ porphyrin group to the modified graphene
133 plane with a Fe-N bond. A (3×3×1) K-point grid is employed for structural optimization and
134 electronic structural calculations. Moreover, DFT-D3 method is adopted to accurately describe
135 the van der Waals force interaction between catalysts and adsorbates [32]. FeN₄, FeN₅, and
136 other molecules such as H₂O₂ and H₂ are put in the same box. The vacuum layer thickness of
137 20 Å is set in the z-direction to avoid the influence of the interaction between adjacent periodic
138 structures. The solvent effects were accounted by using an implicit solvation model as
139 implemented in the DFT code VASP [33]. The adsorption energy E_{ad} is defined as $E_{ad} = E_{sa} -$
140 $E_{cs} - E_{as}$, where E_{sa} , E_{cs} , and E_{as} is the total energy of substrate with adsorbates, the total energy
141 of the clean substrate, and the total energy of adsorption species, respectively. Fe K edge
142 theoretical XANES spectra of the DFT optimized structures were simulated using the finite
143 difference method (FDM), which was implemented within the Finite Difference Method Near
144 Edge Scattering (FDMNES) package developed by Joly [34]. Broadening contributions from
145 the core-hole lifetime, the inelastic plasmon interaction with photoelectron, the resolution of
146 the beamline, and the Fermi energy was accounted for using an arctangent convolution [35].

147 **2.3 Examination of catalysts**

148 Batch experiments were performed to test the Fenton activities of FeN₅/NG catalyst. The
149 stock solution of phenol (200 mg/L) was prepared by dissolving 200 mg phenol in 1 L of

150 anaerobic deionized water. The phenol removal efficiency in the FeN₅/NG, FeN₄/NG+H₂O₂,
151 FeN₅/NG+H₂O₂, NG+H₂O₂, and homogeneous Fenton (Fe²⁺+H₂O₂) systems are compared.
152 Typically, 2 mg of catalysts were added into 20 ml of a 20 mg/L phenol solution for 30 min to
153 reach the adsorption-desorption equilibrium in the heterogeneous system. The Fenton-like
154 reaction was initiated by adding 10 mmol/L of H₂O₂ aqueous solution. The same amount of
155 Fe²⁺ (Fe²⁺ used in the experiment is FeSO₄) as in FeN₅/NG was added to the homogeneous
156 system. The effect of pH/ H₂O₂ dosage on phenol degradation was evaluated by mixing 20 mg
157 FeN₅/NG with 200 mL phenol solution (20 mg/L) with different initial pH values/added H₂O₂
158 dosages. A 5-mL suspension was taken at fixed time intervals for each batch of the experiment
159 and then filtered to measure phenol concentration. 0.5 mL of isopropanol (IPA) was added after
160 the samples were taken in all batch experiments to prevent further reaction of the ROS with
161 phenol in solution. Ten cycling tests were carried out to investigate the reusability of the
162 FeN₅/NG for the degradation of phenol. The recycled catalyst was treated with UV irradiation
163 before the next Fenton-like reaction.

164 The concentration of phenol was monitored by measuring its absorption at 280 nm using
165 an ultraviolet (UV)-visible (vis) spectrophotometer (TU-1901, Beijing Puxi Inc., China). The
166 electron spin resonance (ESR) measurements were performed on a Miniscope MS-5000 ESR
167 spectrometer (Germany), using 5, 5-Dimethyl-1-pyrrolidine-N-oxide (DMPO), dimethyl
168 sulfoxide (DMSO), and 4-Amino-2,2,6,6-tetramethylpiperidine (TEMP) as the spin-trapping
169 agents for reactive oxygen species (ROS). Radical quenching experiments were carried out to
170 further ascertain the ROS during phenol degradation. IPA (2 mL) and p-benzoquinone (BQ; 15
171 mg) were chosen as scavengers of •OH and superoxide radical (•O₂⁻), respectively. The
172 experimental details for ROS capture processes were similar to the batch catalytic experiment.
173 The PMSO and its oxidation product (phenyl methyl sulfone; PMSO₂) were identified by an
174 Agilent 1200 high-performance liquid chromatography (HPLC). The cumulative •OH
175 formation in different systems was quantified with the benzoic acid method [36]. 5.87 was used

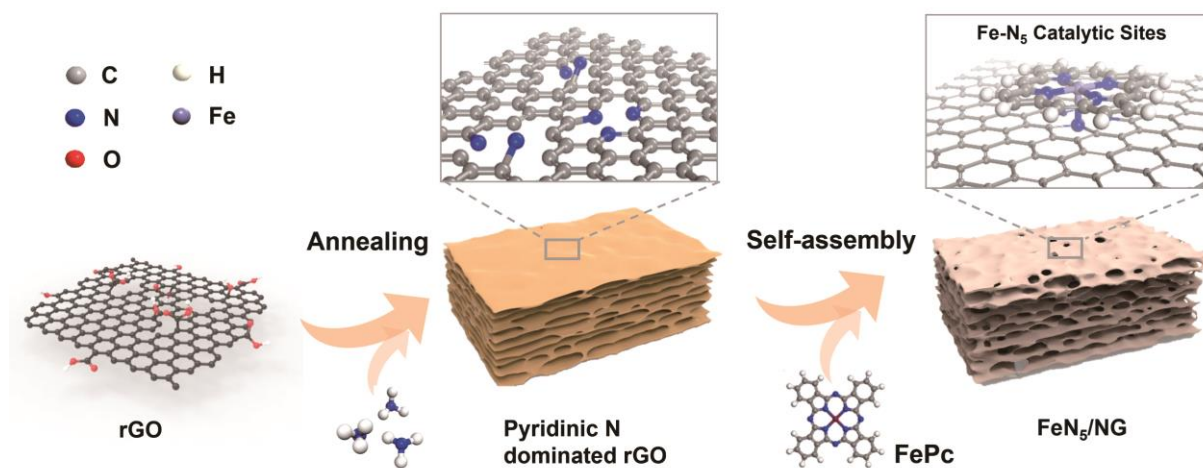
176 as the conversion factor for the estimation of the cumulative $\bullet\text{OH}$ from *p*-hydroxybenzoic acid
177 (*p*-HBA). The oxidation product of BA, *p*-HBA, was quantitatively analyzed using a HPLC
178 (Alliance 2695, Waters, USA) with an ACQUITY UPLC@BEH C18 column (2.1×50 mm, 1.7
179 μm , Waters, USA). The mobile phase was a mixture of 0.1 % trifluoroacetic acid (TFA)
180 aqueous solution-acetonitrile (60:40, v/v).

181 **3. Results and Discussion**

182 **3.1. Characterization of FeN₅/NG**

183 Fig. 1 illustrates the synthesis protocol of FeN₅/NG composites. In this approach, the NG
184 was firstly obtained from rGO annealed at 600 °C in an Ar/NH₃ mixture atmosphere. The as-
185 synthesized NG shows highly crumpled sheet-like morphology (Fig. S1, Supporting
186 Information), in which pyridinic N is strikingly enriched (up to 76.8% of the total nitrogen
187 content for NG; Fig. S2 and Table S3). Afterward, the atomically dispersed metal precursor,
188 FePc, was thoroughly mixed with NG in an aqueous solution and self-assembled with pyridinic
189 N sites in NG via strong π - π interactions. The pyridinic N, as the axial ligand, changes the
190 coordination number of Fe center [37,38], and the atomically dispersed Fe-N₅ catalytic site in
191 NG can be obtained after a lyophilization process. Such a pyrolysis-free synthesis approach is
192 moderate without harsh reaction condition, which is crucial to a controlled modulation of
193 coordination environment around the active site.

194 TEM and SEM images of FeN₅/NG show similar morphology of the NG with flakelike
195 layer and wrinkled structure (Fig. 2a and Fig. S3). The interplanar spacing is estimated to be
196 0.35 nm in the high-resolution TEM (HR-TEM) image, which is attributed to typical (002) basal
197 planes in the graphene layer (Fig. 2a). Raman spectra of both NG and FeN₅/NG samples present
198 typical D band ($\approx 1318\text{ cm}^{-1}$) arising from the defects in graphitic lattice and G band (≈ 1580
199 cm^{-1}) arising from the in-plane vibration of the sp^2 carbon framework (Fig. S4), indicating that
200 NG morphology changes with FePc attached are negligible. The PXRD pattern of FeN₅/NG
201 exhibits two wide peaks at $2\theta \approx 24^\circ$ and 44° , corresponding to the (002) and (100) diffraction



202

203 **Fig. 1.** Schematic illustration for the synthesis of FeN₅/NG.

204

205 planes of graphite, respectively (Fig. S5), which is further evidenced by the selected area
 206 electron diffraction (SAED) pattern (inset of Fig. 2a). No metal-related pattern is detected,
 207 ruling out the undesirable formation of metallic particles or aggregates. With aberration-
 208 corrected STEM, a large number of atom-scale bright spots that represent single Fe atoms are
 209 identified (Fig. 2b). We do not find nanoparticle/nanocluster in the whole region of STEM
 210 images which are selected randomly (Fig. S6), in accordance with the PXRD results. The
 211 intensity profiles of HAADF image over traces marked with orange and green show only one
 212 maximum peak, indicating the single atomic state of Fe specie (Fig. 2c). EDS element mappings
 213 reveal the homogeneous dispersion of Fe atoms on the NG, with the observed overlapping
 214 distribution of Fe, C, and N in Fig. 2d. The atomic ratio of Fe on FeN₅/NG is determined to be
 215 1.97 wt% by EDS quantitative analysis, being consistent with the overall compositional analysis
 216 with ICP-OES (Table S4).

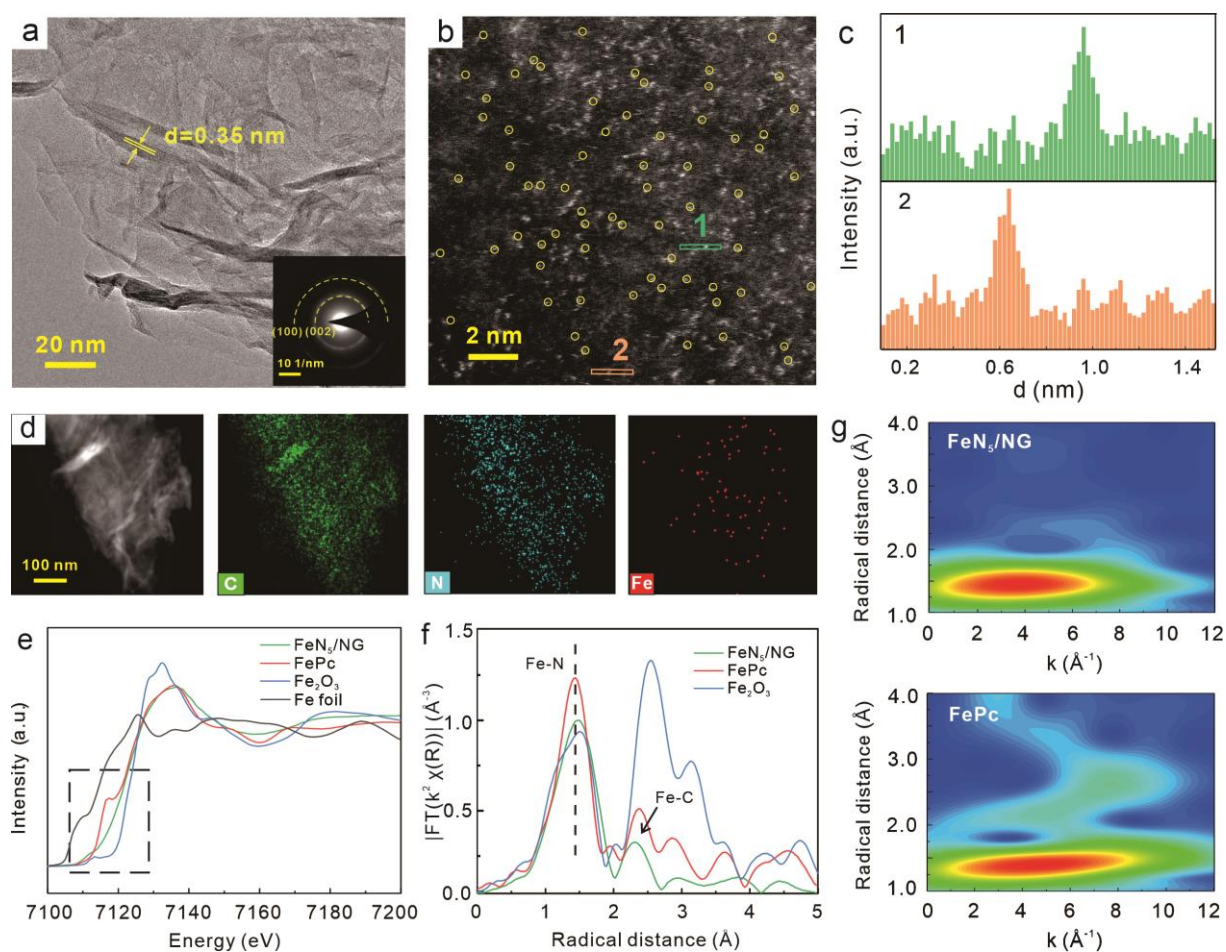
217 To further identify the local coordination environment of single-atom Fe in FeN₅/NG,
 218 several spectral analyses were carried out. Wide scan XPS (Fig. S7) shows the occurrence of C,
 219 N, O, and Fe elements in FeN₅/NG. The C species can be classified into four types: C–C (284.5
 220 eV), C–N (285.4 eV), C–O (286.2 eV), and C=O (288.5 eV). N 1s XPS spectrum can be

221 deconvoluted into four groups with peaks at 398.2, 399.5, 399.9, and 400.8 eV, assigned to
222 pyridinic N, pyrrolic N, Fe-N_x, and graphitic N. The obvious decrease in the ratio of pyridinic
223 N (71.3%) in FeN₅/NG compared to NG (76.8%) (Table S3), along with the emergence of Fe-
224 N_x species, indicates the coordination of pyridinic N with Fe atoms in the catalyst. The Fe 2p
225 XPS spectrum of FeN₅/NG reveals that Fe²⁺ is the predominant Fe speciation in the sample, as
226 indicated by the relative area ratio of the peaks assigned to Fe²⁺ and Fe³⁺ of 77.9% and 22.1%,
227 respectively. The Mössbauer spectroscopy is further conducted to discriminate the coordination
228 structure of Fe atoms. The spectrum of FeN₅/NG can be fitted into three doublets (D1-D3). The
229 doublets D2 and D3 are assigned to medium-spin X-Fe³⁺N₄-Y sites (X and Y refer to O or N
230 ligand) and low-spin FePc-like Fe²⁺N₄, respectively [39, 40]. D3 can be attributed to N-
231 (Fe²⁺N₄) medium-spin species with a penta-coordinated rhombic monopyramidal structure [40].
232 The relative absorption area (73.2%) of the second doublet indicates the high content of Fe-N₅
233 catalytic site in FeN₅/NG (Fig. S8). Such chemical state of Fe atoms is also verified by XAS.
234 As shown in Fig. 2e, Fe K-edge X-ray absorption near-edge structure (XANES) spectrum of
235 FeN₅/NG shows typical features of the blunt white line and weak oscillations for single atom
236 samples. The larger pre-edge shoulder for the square planar structure of FePc disappears,
237 indicating the reconstruction of the coordination structure around Fe atoms. The raising edge
238 of FeN₅/NG is located between the ones for FePc and Fe₂O₃ (marked with the dashed box) with
239 a linearly fitted valance state of +2.3 (Fig. S9), well consistent with the XPS results. Fourier
240 transformed (FT) Fe K-edge extended X-ray absorption fine structure (EXAFS) shows a
241 scattering peak at ~ 1.44 Å for FeN₅/NG, which represents the Fe-N coordination bonds from
242 both FePc and Fe-NG (Fig. 2f). The bond length for FeN₅/NG is slightly larger than the one in
243 FePc, which is due to longer Fe-N coordination bond and/or the stretched FePc coordination,
244 in accordance with the DFT optimized structure (Fig. 2f and Fig. S10). The characteristic peak
245 representing Fe-C second coordination shell is maintained, indicating the preservation of FePc
246 structure. Together with the faded pre-edge shoulder, this result indicates that FePc is anchored

247 to NG as a molecular complex, and thus should give rise to N-axial coordinated Fe–N₅
248 coordination structure. This is confirmed by both XANES simulations and EXAFS fitting,
249 which provide theoretical spectrum of FeN₅/NG with aligned features and well-matched fitting
250 with 5.86±1.48 average Fe–N coordination number, respectively (Fig. S11 and Table S5). The
251 larger first shell Fe coordination number may come from the adsorption of gas molecules in the
252 atmosphere. The wavelet transform (WT) plot of FeN₅/NG shows the WT maximum at 3.7 Å⁻¹,
253 corresponding to the Fe–N bonding compared with Fe₂O₃, Fe foil, and FePc (Fig. 2g and Fig.
254 S12). The insignificant shell of Fe backscatters at ~2.18 Å corresponding to Fe–Fe coordination
255 suggests that that atomic Fe sites are predominantly present without aggregation. In addition,
256 the isolated site dominated with Fe–N₄ coordination structure in the FeN₄/NG obtained by the
257 pyrolysis process of FeN₅/NG is confirmed (Fig. S13, Table S5).

258 **3.2. Fenton-like performance of FeN₅/NG in wastewater treatment**

259 To examine the catalytic role of Fe–N₅ coordination, the Fenton activity of FeN₅/NG is
260 systematically evaluated. Phenol, a typically volatile organic contaminant, is selected as a
261 model contaminant considering its environmental risk. As shown in Fig. 3a, the phenol removal
262 performance of H₂O₂, FeN₅/NG, FeN₄/NG+H₂O₂, FeN₅/NG+H₂O₂, NG+H₂O₂, and
263 conventional homogeneous Fenton (Fe²⁺+H₂O₂) systems at room temperature are compared.
264 We note that H₂O₂ cannot degrade phenol in 25 min, while phenol removal efficiency for
265 FeN₅/NG only reaches 19.8% in the absence of H₂O₂. Comparatively, the phenol removal
266 efficiency of 99.8% in 25 min is observed for FeN₅/NG after adding H₂O₂. Such a high phenol
267 removal rate of FeN₅/NG far exceeds that of FeN₄/NG catalyst and homogeneous systems, as
268 seen from the first-order reaction rate constant (*k*_{obs}) of 0.180 min⁻¹ for FeN₅/NG, which is 3.3
269 and 4.1 times higher than that of FeN₄/NG (0.054 min⁻¹) and homogeneous Fenton process
270 (0.038 min⁻¹), respectively (Fig. 3b). Noting that adsorption is the first and an important step
271 in Fenton-like degradations of contaminants, and high adsorption facilitates the mass transfer

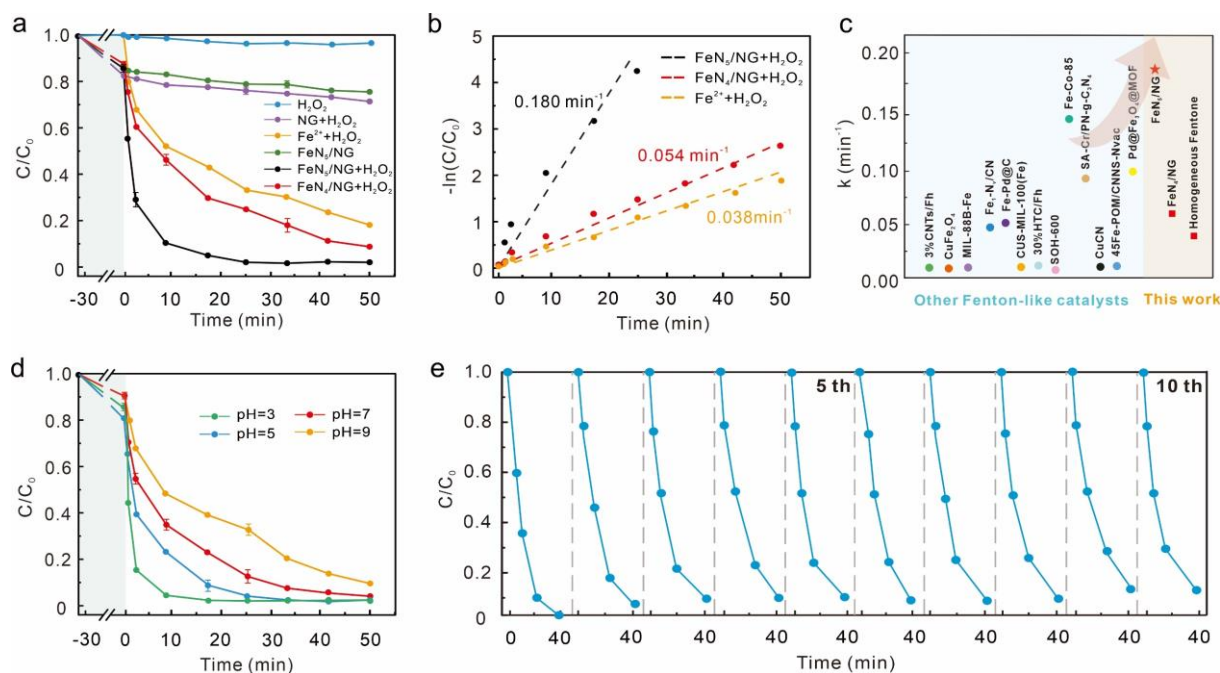


272
 273 **Fig. 2.** Characterization of the FeN₅/NG catalyst. a–b) TEM image (a) and HAADF-STEM
 274 images (b) of the FeN₅/NG catalyst. Inset in (a) is SAED of FeN₅/NG catalyst. c) The height
 275 profile of Fe single atoms marked in (b). d) EDS mapping (C, N, and Fe) of the FeN₅/NG
 276 catalyst; e) Fe K-edge XANES spectra of the FeN₅/NG, Fe foil, FePc, and Fe₂O₃. f) FT of the
 277 Fe K-edge EXAFS of the FeN₅/NG, Fe₂O₃, and FePc. g) WT analysis of the Fe K-edge EXAFS
 278 spectra of the FeN₅/NG (top) and FePc (bottom).

279
 280 of contaminants to the catalysts and driving their oxidative degradation. During this step,
 281 FeN₅/NG has similar adsorption behavior to FeN₄/NG, while showing better adsorption
 282 capacity and efficiency than FeN₄/G (Fig. S14). Above results highlight the key roles of the N
 283 species on NG as the adsorption site for contaminants and axial anchoring site for FePc toward
 284 enhanced phenol removal of FeN₅/NG. In addition, FeN₅/NG exhibits more superior Fenton-

285 like performance as comparing with most other state-of-the-art heterogeneous catalysts (Fig. 3c
286 and Table S6). The total organic carbon (TOC) degradation rate within 50 min is over 95% in
287 the FeN₅/NG+H₂O₂ system (Fig. S15), demonstrating the excellent mineralization ability of
288 FeN₅/NG. Only a minor amount of Fe (< 0.8 mg/L) is leached during the reaction (Fig. S16),
289 which meets the permissible limit of Fe (5 mg/L) according to the Environmental Quality
290 (Sewage and Industrial Effluents) Regulation 1979 [41].

291 Further experiments are conducted to explore the versatility of FeN₅/NG for phenol
292 removal under different reaction conditions. Fig. 3d reveals the high Fenton activity of
293 FeN₅/NG over a wide pH range, that over 91.2% of phenol can be degraded within 50 min in
294 the pH range of 3–9. Such a broad operating pH for FeN₅/NG is not achievable with most
295 advanced Fenton-like catalysts [42-44]. The removal efficiency is improved from 78.5 to 99.9%
296 in 50 min as the H₂O₂ dosage increased from 2.5 to 20 mmol/L (Fig. S17), due to the
297 participation of H₂O₂ as a precursor in the Fe²⁺/Fe³⁺ redox cycle, according to the Haber-Weiss
298 mechanism [45]. Recycling experiment was carried out to investigate the stability of FeN₅/NG
299 as a Fenton-like catalyst (Fig. 3e). Although the degradation efficiency slightly decreased as
300 the number of cycles increased, good reusability still remains even after 10 cycles (99.0%
301 degradation of phenol within 40 min). Moreover, only 9% of TOC remains after 10 cycles of
302 catalytic reactions, which is much less than that of the conventional homogeneous Fenton
303 system (52%) (Fig. S18). Noting that the mass loss of FeN₅/NG is less than 0.5 wt % after the
304 10th cycle (Table S7) and that the microstructure is almost unchanged (Fig. S19), FeN₅/NG
305 shows a high stability in catalyzing Fenton-like process. A slight increase in the relative content
306 of Fe(III) 22.1% to 26.3% and a decrease in the relative content of Fe(II) from 77.9% to 73.7%
307 is observed after the recycling experiment (Fig. S20), which can be explained that the rate of
308 H₂O₂ with Fe(III) is slower (0.001–0.01 m⁻¹·s⁻¹) than Fe(II) oxidation by H₂O₂ (40 m⁻¹·s⁻¹).
309 The conversion of Fe species in FeN₅/NG might lead to less generation of ROS, which results
310 in the declined activity of FeN₅/NG with increasing cycle.

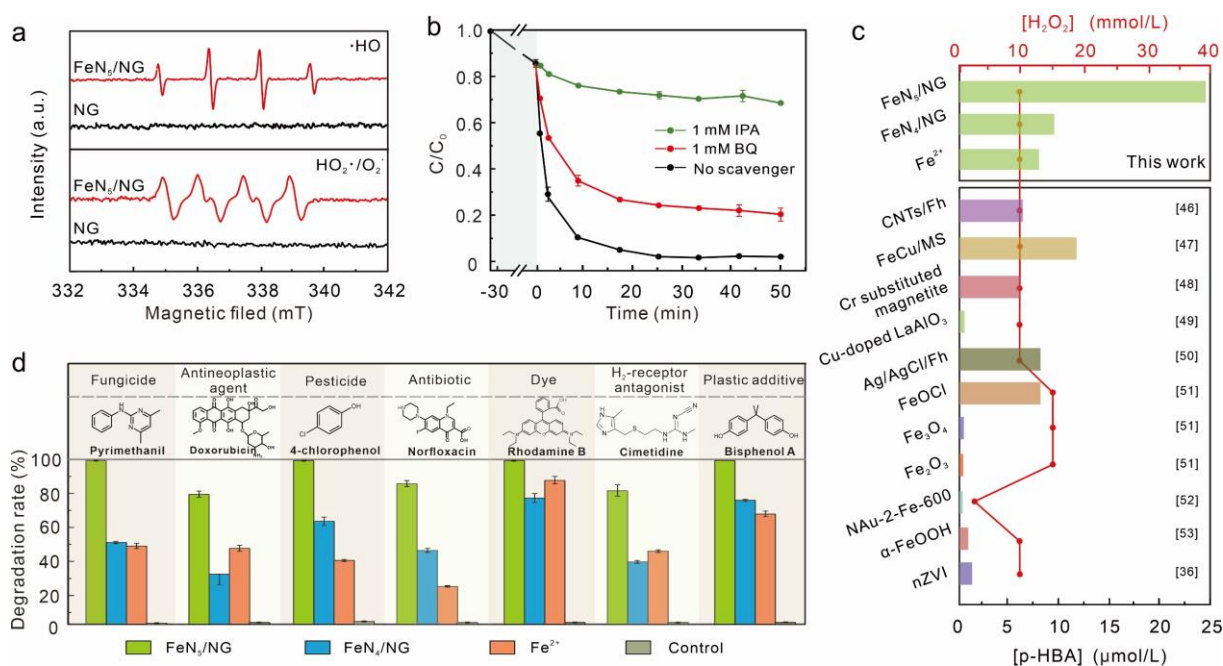


311
 312 **Fig. 3.** Fenton activity of FeN₅/NG catalyst. a) Phenol degradation behavior of different
 313 catalysts (pH= 4.0 ± 0.2, [Catalyst]= 0.1 g/L, [phenol]= 20 mg/L, [H₂O₂] = 10 mmol/L). b) The
 314 corresponding kinetic plots for the phenol degradation with different catalysts. c) Comparison
 315 of the kinetics of organic contaminants degradation by recently reported state-of-the-art
 316 catalysts. d) The phenol degradation by FeN₅/NG at different pH values. ([Catalyst]=0.1 g/L,
 317 [phenol]= 20 mg/L, [H₂O₂]=10 mmol/L). e) Stability of the FeN₅/NG for the degradation of
 318 phenol ([phenol]=20 mg/L; The recovered samples were pretreated with UV irradiation only
 319 before the Fenton reaction).

320

321 3.3. Dual-center mechanism for accelerating phenol degradation

322 The ROS contributing to phenol degradation are identified by ESR and radical quenching
 323 experiments to understand the removal mechanism. As shown in Fig. 4a, the signal of •OH
 324 captured by DMPO with four characteristic peaks in a ratio of 1:2:2:1 and the signal of
 325 HO₂•/O₂⁻ captured by DMSO with characteristic 1:1:1:1 quadruple peak are observed, in the
 326 appearance of •OH and HO₂•/O₂⁻ in the FeN₅/NG+H₂O₂ system. The minor detection of the
 327 signals for ¹O₂ by TEMP spin trapping in both FeN₅/NG-H₂O₂ and FeN₄/NG-H₂O₂ system rules



328

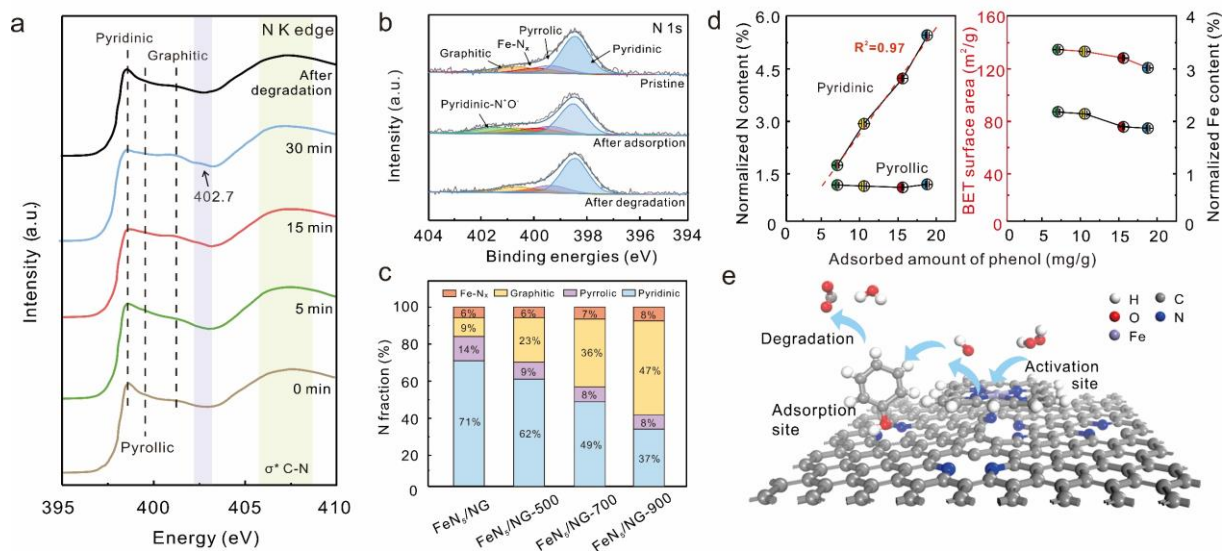
329 **Fig. 4.** Generation and detection of ROSs on FeN₅/NG. a) ESR spectra for the detection of $\cdot\text{OH}$
 330 (top) in the presence of DMPO and $\text{HO}_2\cdot/\text{O}_2^-$ (bottom) in the presence of DMSO. b)
 331 Degradation curves of phenol in the presence of different radical scavengers, IPA and BQ
 332 ($[\text{phenol}] = 20 \text{ mg/L}$, $[\text{IPA}] = 2 \text{ mL}$, $[\text{BQ}] = 15 \text{ mg}$). c) The concentration of p-HBA in 5 min of
 333 different Fenton-like reaction catalysts. d) Degradation of select organic pollutants in
 334 FeN₄/NG+H₂O₂, FeN₅/NG+H₂O₂, conventional homogeneous Fenton (Fe²⁺+H₂O₂), and control
 335 (H₂O₂) systems. ($\text{pH} = 4.0 \pm 0.2$, $[\text{Catalyst}] = 0.1 \text{ g/L}$, $[\text{organic pollutant}] = 20 \text{ mg/L}$, $[\text{H}_2\text{O}_2] =$
 336 10 mmol/L , reaction time = 40 min).

337

338 out the possibility of nonradical ROS as the dominant oxidant during phenol degradation (Fig.
 339 S21). In addition, almost no PMSO₂ was detected in the FeN₅/NG-H₂O₂ system, which implies
 340 that the Fe(IV) species is barely involved in the reaction (Fig. S22). The radical quenching
 341 experiments utilized IPA for $\cdot\text{OH}$ scavenger and BQ as the $\text{HO}_2\cdot/\text{O}_2^-$ scavenger. As seen from
 342 Fig. 4b, the degradation behavior of phenol by FeN₅/NG slightly decreases in 50 min (down to
 343 77.2 %) after addition of BQ, while the deactivation of catalyst is prominent in the presence of
 344 IPA (down to 29.7%). This proves that the $\cdot\text{OH}$ contributes more than $\text{HO}_2\cdot/\text{O}_2^-$ to the

345 decomposition of phenol. With these results, the major ROS generated at the Fe–N₅ active site
346 for phenol oxidation is therefore confirmed to be •OH. Cumulative •OH formed in the
347 FeN₅/NG+H₂O₂ system measured with BA as an •OH probe reaches 142.6 μmol/L in 5 min,
348 which is higher than that in FeN₄/NG and homogeneous Fenton systems (Fig. 2f),
349 correspondingly explaining the optimal phenol degradation efficiency of FeN₅/NG. Moreover,
350 the formed p-HBA of FeN₅/NG, to the best of our knowledge, is the highest at the room
351 temperature among other Fenton-like reagents reported so far (Fig. 4c) [46-53], which translates
352 into the excellent oxidative degradation of various other organic contaminants (Fig. 4d).

353 In general, the adsorption of target contaminant by Fenton-like catalyst is an important
354 property in determining the degradation performance [54]. In this regard, ascertaining the
355 adsorption-degradation process of phenol by FeN₅/NG is necessary for gaining a deeper insight
356 into the structure-property relationship. N K-edge XAS is performed to monitor the
357 coordination structure evolution of FeN₅/NG during the Fenton-like reaction. As illustrated in
358 Fig. 5a, the initial N K-edge XANES spectra of FeN₅/NG suspension without phenol exhibits
359 three peaks at around 398.3, 399.2, and 400.8 eV, arising from the electron excitation from N
360 1s orbital into antibonding π* states of pyridinic N, pyrrolic N, and graphitic N species,
361 respectively [55]. The order of relative energy positions of these N species are consistent with
362 the XPS results discussed at the beginning. Continuous adsorption of phenol by NG results in
363 the transformation of pyridinic N species on NG, as revealed by the decreased intensity of the
364 pyridinic N peak and the appearance of the new peak at ~402.7 eV after 30 min of adsorption
365 (Fig. 5a). Similar results can be obtained by the XPS characterization, with N 1s spectra of
366 FeN₅/NG showing a remarkable decrease in the content of pyridinic N and formation of new
367 pyridinic-N⁺O⁻ species (402.2 eV) after adsorption (Fig. 5b) [56]. After the addition of H₂O₂ to
368 degrade phenol, both N K-edge XAS and N 1s XPS spectra were restored back to the initial
369 state, which indicates that pyridinic N are important phenol adsorption sites for FeN₅/NG. It



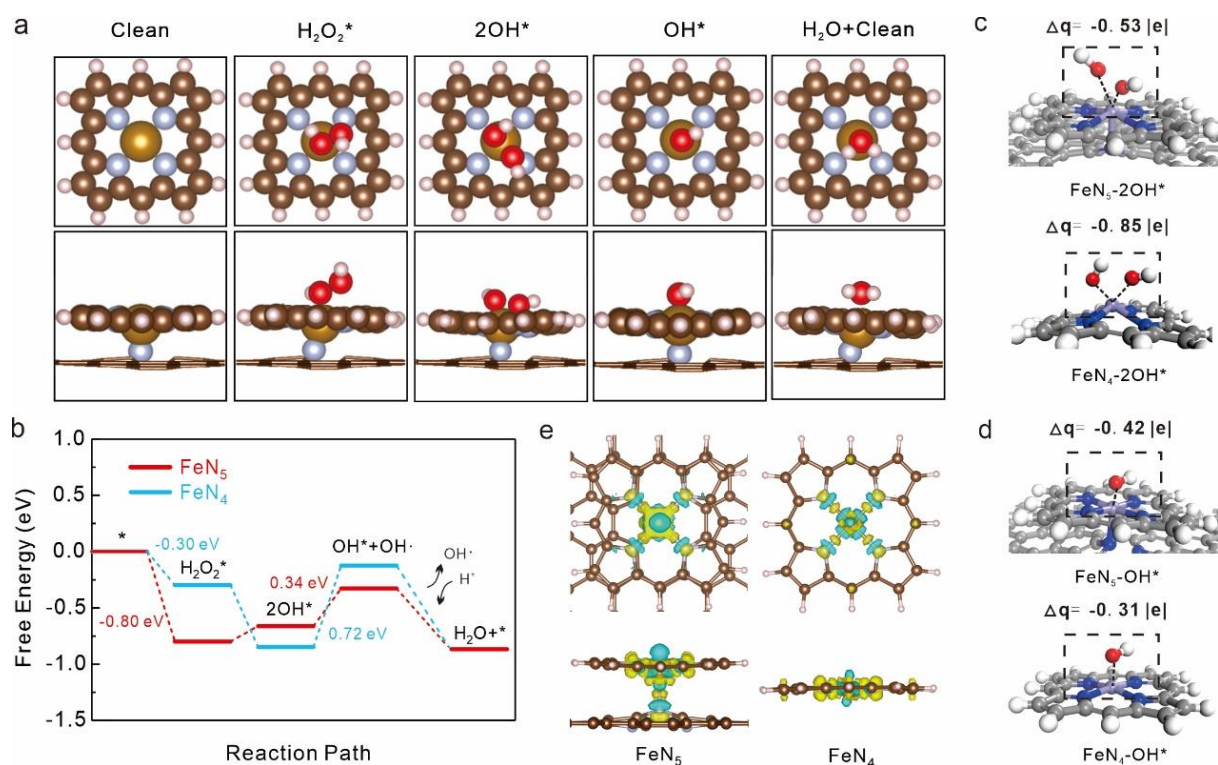
370
 371 **Fig. 5.** Phenol adsorption properties of FeN₅/NG. a) N K-edge XANES spectra of FeN₅/NG at
 372 different stages of phenol adsorption. b) N 1s XPS spectra in FeN₅/NG at pristine state, after
 373 phenol adsorption, and after phenol degradation. c) The relative contents of different N species
 374 in FeN₅/NG, FeN₅/NG-500, FeN₅/NG-700, and FeN₅/NG-900. d) The relationship between the
 375 adsorbed amount of phenol and the normalized contents of pyrrolic N, pyridinic N, and Fe, as
 376 well as the BET surface area. e) Schematic illustration of the dual reaction sites catalytic
 377 pollution control mechanisms of FeN₅/NG.

378
 379 can be explained that each pyridine N site contains an unpaired electron, which is most readily
 380 form a σ bond in this system by pairing with a 2p electron of O atom on phenol and then forms
 381 pyridine-N⁺O⁻ species, as supported by DFT calculations showing the highest adsorption energy
 382 (E_{ads} ; 2.8 eV) for pyridinic N with O atom as compared to other atoms on phenol (Fig. S23).
 383 The correlation between the pyridinic N and adsorption ability of FeN₅/NG is further
 384 investigated by adjusting the calcination temperature of NG to tailor the amounts of pyridinic
 385 N. The relative contents of N species on different catalysts determined by XPS analysis reveal
 386 that increasing calcination temperature of NG leads to the conversion of pyridinic N to graphitic
 387 N, as seen that the ratio of pyridinic N in the catalysts decreases to 37% after calcination of the
 388 NG carrier at 900 °C (Fig. 5c and Fig. S24). The normalized content of pyridinic N on the

389 catalyst has a positive linear relationship with the amount of adsorbed phenol ($R^2 = 0.97$; Fig.
390 5d). Conversely, no apparent correlation is observed cd content of Fe and pyrrolic N as well as
391 the BET surface area with the phenol adsorption ability (Fig. 5d). Therefore, the pyridinic N on
392 FeN₅/NG should be the primary adsorption site for phenol, and the dual-center mechanism, that
393 is, the pyridinic N site on NC is the phenol adsorption center and the Fe–N₅ site is the H₂O₂
394 activation center, can be proposed to achieve phenol removal (Fig. 5e). It is worth mentioning
395 that the effective adsorption of phenol onto the pyridinic N site on FeN₅/NG results in a decrease
396 in the migration distance of •OH generated from nearby Fe–N₅ sites, which could dramatically
397 improve the overall phenol degradation performance.

398 **3.4. Coordination-dependent nanostructure for Fenton activity**

399 To probe the underlying coordination-dependency of Fe single atoms in Fenton catalysis,
400 DFT calculations are utilized to simulate the H₂O₂ activation process at optimized Fe–N_x (x=4
401 or 5) configurations. Noting that the •OH is validated as the primary ROS in this study, a H₂O₂
402 activation pathway under the acidic catalytic milieu is therefore investigated (Fig. 6a). Firstly,
403 the H₂O₂ molecule is adsorbed onto the Fe–N_x active site, which easily undergoes O–O cleavage
404 and then forms two OH* groups. Subsequently, one OH* group desorbs from the adsorbed site
405 to produce an •OH, while the residual OH* can easily reacts with H⁺ to form the H₂O product
406 [57]. The Gibbs free energy diagrams and the stepwise atomic structures for intermediates on
407 the Fe–N_x site are summarized (Fig. 6b and Fig. S25, 26). It is noticed that the E_{ads} for H₂O₂ on
408 the Fe–N₄ and Fe–N₅ active sites are 0.30 and 0.80 eV, respectively, revealing that the
409 interaction of Fe–N₅ active site with H₂O₂ is stronger than that of Fe–N₄ site. The dissociation
410 of one OH* group to generate a reactive •OH is the rate-determining step (RDS), with the free
411 energy increases of 0.34 and 0.72 eV for Fe–N₅ and Fe–N₄ models, respectively. Bader charge
412 analysis shown in Fig. 6c reveals that the 2OH* intermediate accepts electrons of 0.53 and 0.85
413 |e| from the Fe–N₅ and Fe–N₄ sites, respectively, indicating that the FeN₅/NG has less charge
414 transfer between the adsorbed OH* and the Fe active center. It can be explained that, unlike



415
 416 **Fig. 6.** Fenton activities of coordination-regulated Fe single atoms. a) Proposed Fenton-like
 417 reaction process on FeN₅/NG under acidic environment. b) Energy diagram of the reaction
 418 process for FeN₅ and FeN₄ models. c-d) Configurations and Bader charge of the adsorption of
 419 two OH groups (c) and one OH group (d) on the FeN₅/FeN₄ models. e) Charge density
 420 differences of FeN₅ and FeN₄ models. The yellow and skyblue regions represent electron
 421 accumulation and electron depletion, respectively.
 422
 423 the Fe–N₄ site in which the Fe atom reaches coordination saturation after adsorption of two
 424 OH* groups, the six-coordinated Fe atom can only contribute to the strong tendency for FeN₅
 425 to interact with one single OH* group in the 2OH* step, as the significant difference in charge
 426 transfer amount from FeN₅ to the two different OH* groups (0.05 vs 0.48 |e|; Fig. S27).
 427 Moreover, the charge transfer from Fe–N₅ site to OH* (-0.42 |e|) is more than that of Fe–N₄ site
 428 (-0.31 |e|) in the FeN₅/FeN₄-OH* system (Fig. 6d). A significant difference in bonding charge
 429 distribution is observed between the Fe atom and surrounding N atoms at the Fe–N₄ and Fe–N₅
 430 sites, which reveal the nature of different charge-transfer properties in the H₂O₂ activation

431 process (Fig. 6e). Therefore, one OH* group is more easily to dissociate from the Fe–N₅ site
432 and then form the free •OH. The enhanced catalytic ability of FeN₅/NG is closely related to its
433 higher ability to adsorb H₂O₂ molecules (larger adsorption energy) and its higher ability to
434 generate •OH (lower energy barrier).

435 **4. Conclusion**

436 In summary, we report a pyrolysis-free and coordination-modulated method to obtain a Fe
437 SAC with axial five-coordinated structure (Fe–N₅) for catalytic oxidation of organic
438 contaminants. The obtained FeN₅/NG is demonstrated to exhibit efficient formation of the
439 active species (mainly •OH), thus showing favorable Fenton activity towards catalytic oxidation
440 of phenol with a degradation rate constant of 0.180 min⁻¹. DFT calculations reveal the
441 dependence of catalytic reactivity on the coordination environment of Fe single-atom, showing
442 that the Fe–N₅ catalytic site more readily adsorbs the H₂O₂ and generates •OH compared to the
443 Fe–N₄ site. Moreover, a novel dual-center mechanism has been proved for understanding the
444 impressive catalytic performance, in which the pyridinic N site on NG serves as the phenol
445 adsorption center and the Fe–N₅ sites serves as the H₂O₂ activation center. Such dual reaction
446 centers facilitate the rapid reaction of •OH generated by H₂O₂ activation with neighboring
447 adsorbed phenol. This work presents a new avenue to regulate the local coordination
448 environment of SACs and establishes the foundation for a detailed understanding of the
449 relationship between the catalyst structure and Fenton activity for further research.

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