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Green preparation of silk nanofiber membranes from natural silkworms for effective dye/salt fractionation

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19 **Abstract**

20 While membranes are widely used in sustainable separations, they are mostly made from
21 petroleum-based polymers and toxic solvents, which are not only harmful to the environment,
22 but also pose a major risk to the safety and health of people. Aiming to enhance the
23 sustainability of fabricating membranes, a biobased silk nanofiber (SNF) membrane is uniquely
24 developed from natural silkworms using green solvents and pressure-assisted deposition
25 method for dye/salt fractionation. One key feature is the replacement of traditional toxic
26 solvents used for SNF extraction to a green solvent, deep eutectic solvent (DES) which is
27 utilized and recycled for SNF preparation. The use of DES can effectively weaken the bonding
28 to disintegrate the silk fibers into microfibrils without destroying the inherent properties of silk
29 fibers. Various SNF loadings were explored to investigate the self-assembling of SNF and
30 optimize the separation performance. The optimized SNF membrane exhibits a high separation
31 factor of 110.7 and remarkable stability in continuously separating NaCl and rose bengal for
32 100 hours. As compared to the conventional membranes for dye/salt fractionation, the newly
33 developed biobased SNF membrane significantly reduces the environmental hazard by
34 incorporating renewable polymers and green solvents, offering a promising pathway towards
35 the establishment of a sustainable membrane industry.

36

37 **Key words:** Biobased polymers; green solvents; silk nanofibers; deep eutectic solvents;
38 dye/salt fractionation

39 **1. Introduction**

40 Sustainable manufacturing is increasingly popular in companies due to its green strategies, cost
41 reduction in operations and minimized environmental impact [1-3]. Treating industrial
42 wastewater and recycling the valuable components are crucial in the establishment of circular
43 economy in industrial processes [4]. One major wastewater contributor is the textile industry.
44 In China, a daily average of 2 million cubic meter of dye wastewater is discharged which would
45 mean approximately 100,000 tons of dyes and 10 million tons of inorganic salts can be recycled
46 yearly [5]. High concentration of salts are found in wastewater as they are intentionally added
47 to enhance the adhesion of dyes [6]. With membrane technology as an emerging technique, it
48 is effective in tackling the above issues due to its sustainability and efficiency. Its added
49 advantages include low energy consumption, compact and modular design and simple
50 operation [7-9]. Nanofiltration membranes are capable in effectively retain small organic
51 solutes and divalent salts with pore sizes of 0.5-2 nm. However, a significant drawback arises,
52 given that nanofiltration membranes rely on materials derived from fossil resources, such as
53 polysulfone, polyether sulfone, and polyacrylonitrile, for the fractionation of dye and salt
54 mixtures [10-12]. Furthermore, the membrane wastes are typically disposed via landfill or
55 incineration, thus, adding on to the existing soil pollution and greenhouse gases [13-17].

56

57 In accordance with the twelve principles of green chemistry, a blueprint of sustainable circular
58 membrane industry is devised, where renewable polymers and green solvents are used in the
59 fabrication of the membranes [13, 14, 18-21]. Currently, renewable polymers are mostly
60 biobased polymers derived from either bacterial fermentation or vegetables and animals. For
61 example, lignin and cellulose are extracted from plant fibers of wood, cotton, straw and bamboo.
62 Sericin and fibroin are sourced from silk fibers, while chitosan is obtained from chitin, which
63 exists in the outer shells of crustaceans. These materials possess high hydrophilicity,

64 biocompatibility and biodegradability, coupled with low toxicity, carbon footprint and
65 environmental impact [22-24]. However, a dilemma persists concerning the trade-off between
66 the processability and stability of biobased polymers, imposing limitations on their
67 applicability in membranes. Furthermore, with its limitation to produce biobased polymers at
68 production scale and their elevated cost diminishes their economic attractiveness compared to
69 petroleum-based materials [13, 22].

70

71 Natural silk fiber is a natural protein fiber that is commonly extracted from the *Bombyx mori*
72 silkworm cocoon and it is largely used in the textiles for centuries. It consists of two main
73 proteins: 70-80% fibroin and 20-30% sericin, where the fibroin is the structural component and
74 the sericin is the adhesive that holds the fibers together [25]. Silk fibroin is known to be one of
75 the strongest elastomeric biomaterials with remarkable strength, durability and lightweight
76 properties. It is commonly extracted from natural silkworms through degumming and
77 dissolution processes [26]. At present, a variety of acid solvents or aqueous solution of
78 inorganic salts, such as 1,1,1,3,3,3-Hexafluoro-2-propanol (HFIP), N-methyl morpholine N-
79 oxide (NMMO), and hexafluoroacetone hydrate, have been employed to generate silk fibroin.
80 However, most of them are toxic and may destroy the structural hierarchy of silk fibers [27,
81 28].

82

83 To improve the sustainability of membrane fabrication process and reduce the utilization of
84 petroleum-based polymers, herein, we propose a green and facile strategy to prepare a silk
85 nanofiber (SNF) composite membrane for dye/salt fractionation to treat textile wastewater.
86 SNF was first extracted from natural silkworms using a deep eutectic solvent (DES), which is
87 a type of ionic liquid containing large nonsymmetric ions that have low lattice energy and low
88 melting point [29]. It is often regarded as a green solvent due to its low vapor pressure,

89 nonflammability, ease of preparation and good recyclability. Next, SNF was self-assembled
90 onto a cellulose acetate substrate via a pressure-assisted deposition method. Various SNF
91 loadings on the membrane were investigated and the developed membranes were found to
92 exhibit excellent separation performance and stability in fractionating dye/salt mixture for
93 resource recovery in textile industries. Moreover, it is envisioned that the developed SNF
94 composite membrane that utilizes biobased polymers and green solvents can reduce
95 environmental impact, thus contributing to the advancement of sustainable membrane industry.

96

97 **2. Experimental**

98 **2.1 Materials**

99 Choline chloride, sodium carbonate and oxalic acid were purchased from Sigma-Aldrich. B.
100 mori cocoons were purchased from Nanoflux Pte Ltd and were used after removal of the sericin
101 proteins by boiling in an aqueous solution of sodium carbonate. The cellulose acetate
102 membrane substrate (pore size: 0.22 μm) was purchased from Hangzhou Special Paper
103 Industry Co. Ltd. Dopamine hydrochloride (Sigma-Aldrich) was employed to increase the
104 adhesion between silk nanofibers and the substrate. All chemicals were used as received
105 without further purification. In all washing steps, deionized (DI) water (18.2 M Ω) was used.

106

107 **2.2 Preparation of silk nanofibers**

108 B.mori cocoons were degummed in a boiling solution of 0.5 wt% sodium carbonate for 30min.
109 The degummed silk fibers were washed with distilled water and left to dry overnight. The DES
110 was prepared by dissolving equimolar choline chloride (ChCl) and oxalic acid at 80 °C to form
111 a transparent solution. 1g of silk fibers were cut into small pieces and added into the DES. The
112 as-prepared dispersion was mixed and heated to 110°C for 24 h to produce a glue-like
113 dispersion. The produced silk nanofibers were removed and washed using filtration to remove

114 any residue, followed by drying overnight. Silk nanofibers were then re-dispersed in DI water
115 using ultrasonication (Q Sonica, sonicator).

116

117 The recycling of DES was conducted by concentrating the diluted DES solution using a rotary
118 evaporator to remove bulk of the water. It was then further heated in a vacuum oven for 24 h
119 at 60 °C to remove any excess water content in the concentrated DES solution. The recycled
120 DES obtained was weighed to determine the DES recovery percentage after pre-treatment.

121

122 **2.3 Preparation of silk nanofiber composite membranes**

123 Prior to the deposition of silk nanofibers, the cellulose acetate substrate was modified with
124 dopamine to enhance its affinity with silk nanofibers. Dopamine was chosen due to its effective
125 adhesion properties and good biocompatibility. It was expected to aid in the placement of silk
126 nanofibers, thus promoting secure adhesion of the silk nanofibers to the substrate, preventing
127 easy delamination [30, 31]. Initially, 0.2 g of dopamine hydrochloride was dissolved in 100
128 mL of a 0.01M Tris buffer at pH 8.5. Subsequently, the resulting solution was applied to the
129 upper surface of the substrate at room temperature and left for 1 hour. Following this, the
130 substrate was rinsed with DI water to remove the residues.

131

132 The as-prepared silk nanofiber aqueous dispersion was filtered through the dopamine-modified
133 substrate in a dead-end filtration cell at 1 bar by means of a pressure-assisted deposition method.
134 Four types of membranes with different SNF loadings, namely 20.8, 41.6, 83.2 and 124.7 g m⁻²
135 were prepared to optimize the membranes performance, which are labelled as SNM-5, SNM-
136 10, SNM-20 and SNM-30, respectively. The as-prepared composite membranes were cured at
137 60 °C for 5 min in an oven to evaporate residual water. This process facilitated the formation
138 of hydrogen bonds between the silk nanofibers, thereby enhancing structural stability and

139 mitigating the risk of silk nanofiber delamination. The fabricated silk nanofiber composite
140 membranes were then preserved in DI water for further testing.

141

142 **2.4 Characterizations**

143 The morphologies of silk nanofibers and the composite membrane were observed by field
144 emission scanning electron microscopy (FESEM, JEOL JSM7600F). Silk nanofiber aqueous
145 dispersion was dripped onto a silica wafer and vacuum dried. Membrane samples were freeze-
146 dried and fractured in liquid nitrogen. Both samples were coated with a thin layer of gold using
147 a JEOL JFC-1200 coater for FESEM observation. The silk nanofibers and composite
148 membranes were probed using atomic force microscope (AFM) (Bruker JPK NanoWizard 4XP)
149 under the standard tapping mode (in air), with a scanning rate at 0.5 Hz and scan size of 50 x
150 50 μm . The average roughness (R_a) and root-mean-square roughness (R_q) were derived from
151 the triplicates average of R_a and R_q values at different areas, respectively. Transmission
152 electron microscopy (TEM, FEI Titan 80/300 Thermo Fischer Scientific) was employed to
153 observe the silk nanofibers at an accelerating voltage of 200 KV. The hydrodynamic diameter
154 and zeta potential of the silk nanofibers were measured by a dynamic light scattering (DLS)
155 (Zetasizer Nano ZS90) under room temperature. The pristine silk nanofibers, degummed silk
156 nanofibers and the silk nanofiber composite membranes were examined using Fourier
157 transform infrared spectroscopy (FTIR, Bruker Vertex 80v) under attenuated total reflectance
158 mode.

159

160 **2.5 Separation performance for dye/salt fractionation**

161 The pure water permeance (PWP, $\text{L m}^{-2} \text{h}^{-1} \text{bar}^{-1}$, LMH bar^{-1}) of the membrane was evaluated
162 using dead-end filtration cells with a trans-membrane pressure ΔP (bar) of 1 bar at room
163 temperature. The PWP value was determined using the following equation:

$$PWP = \frac{Q}{A\Delta P} \quad (1)$$

164 where Q (L h⁻¹) represents the water flux at the permeate side and A (m²) is the effective
 165 filtration area of the membrane. To ensure consistent measurements, each membrane sample
 166 was assembled and left to stabilize for 1 h before measurement. For each condition, a minimum
 167 of three membrane samples were measured to ensure reliable results and the average results
 168 were reported.

169

170 The rejections to dyes and inorganic salts were determined by preparing feed solutions
 171 containing 50 ppm dyes or 1000 ppm inorganic salts under a trans-membrane pressure of 1 bar
 172 with pre-stabilization of 1 h. The concentrations of dye and salt in both feed (C_f) and permeate
 173 (C_p) were determined using a UV-Vis spectrophotometer (UV-1800 UV/visible scanning
 174 spectrophotometer, Shimadzu) and a conductivity meter (SevenCompact, Mettler-Toledo),
 175 respectively. The dye and salt rejections (R , %) were calculated using Eq. (2).

$$R = \left(1 - \frac{C_p}{C_f}\right) \times 100\% \quad (2)$$

176 The dye/salt fractionation test was conducted using mixed feed solutions containing 50 ppm
 177 rose bengal and 1000 ppm NaCl under 1 bar for 100 h. The separation factor of dye and salt
 178 was determined using the following equation.

$$Separation\ factor_{\frac{Salt}{Dye}} = \frac{x_{Salt}^{permeant} / x_{Dye}^{permeant}}{x_{Salt}^{feed} / x_{Dye}^{feed}} \quad (3)$$

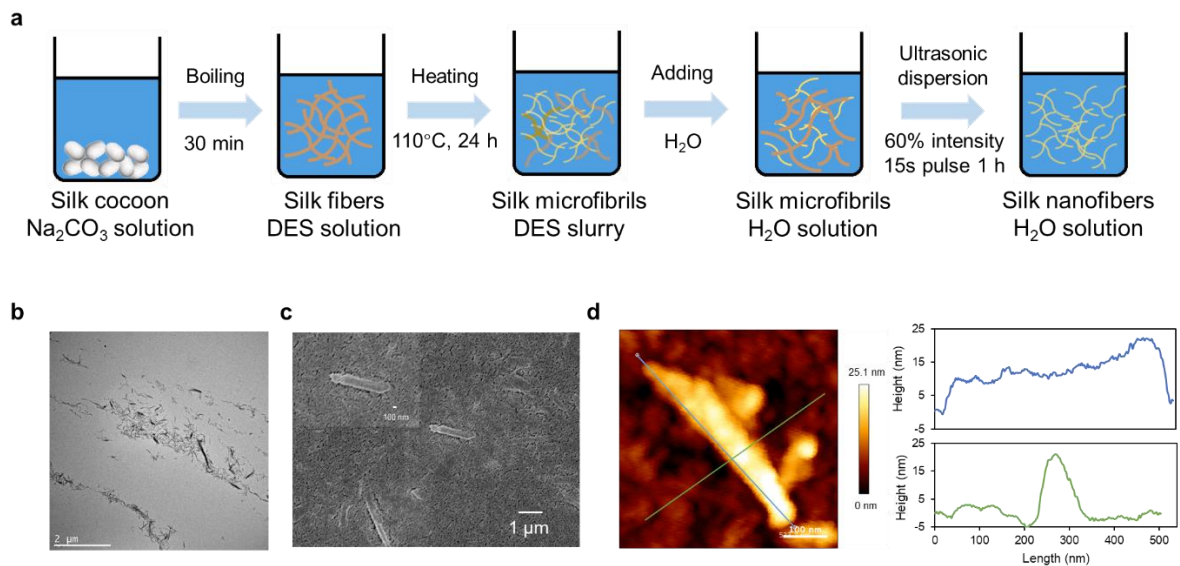
179

180 **3. Results and discussion**

181 **3.1 Synthesis of SNFs and DES recycling**

182 High purity silk nanofibers were obtained via degumming, DES dissolution and ultrasonication,
 183 as illustrated in Fig. 1a. Degumming is an essential step to be carried out as the silk fibers

184 contains sericin, a natural gum like substance which protects the silk fiber structure. This
 185 process is crucial as it breaks the peptide bonds and separate sericin from the fibroin, which is
 186 carried out through hydrolytic degumming using sodium carbonate. After the removal of
 187 sericin, silk fibroin was dissolved into the prepared DES at 110°C. DES is employed as a green
 188 solvent to replace commonly used toxic solvents due to its low toxicity and biodegradability.
 189 DES is a type of ionic liquid that can be formed when a hydrogen bond donor and a hydrogen
 190 bond acceptor are mixed [29]. With its acidity and significant swelling ability, DES can disrupt
 191 the hydrogen bonds and break the fibroin structure to disintegrate the silk fibers into
 192 microfibrils [32]. Silk dissolution is a vital step as it directly affects the characteristics of silk
 193 fibers which impacts the properties of the resulting silk nanofiber. Silk microfibrils were
 194 removed from the DES after dissolution and redispersed in DI water using ultrasonication to
 195 obtain silk nanofibers. The water-dispersible synthesized silk nanofibers facilitate the
 196 subsequent pressure-assisted deposition on the substrate.



197
 198 **Figure 1 Preparation of SNF and its morphology.** a) An illustration of the SNF preparation
 199 steps, which comprises degumming, DES dissolution and ultrasonication processes. b) TEM
 200 image c) SEM images and d) AFM image and depth profile of the prepared SNFs.

201

202 In addition to its low volatility and toxicity, DES can be recycled after silk dissolution and be
203 reused for the next synthesis. As illustrated in Fig. S1, after silk dissolution, the silk fibers are
204 washed with DI water and filtered to remove any excess DES. The diluted DES solution
205 obtained from filtering was then recycled with the use of rotary evaporator and vacuum drying.
206 The recovery percentage of DES is determined to be 78.4% by taking the weight ratio of
207 recovered DES to the initial input for three runs. The good recovery is attributed to the high
208 boiling point and low volatility of DES. This demonstrates DES can serve as an
209 environmentally friendly, economically feasible and sustainable solvent for producing SNFs.

210

211 **3.2 Characterization of SNFs**

212 The morphology and dimension of synthesized silk nanofibers were characterized by TEM,
213 FESEM, and AFM, as shown in Fig. 1b, c and d, respectively. From TEM image (Fig. 1b), the
214 silk fibers can be seen to be mostly disintegrated into fine nanofibers after the degumming,
215 dissolution and ultrasonication. While a few microfibrils still present, there is no large silk
216 fibers observed, indicating that the DES can effectively disintegrate the silk fibers by
217 weakening or partially destroying the strong hydrogen bonds. In addition, ultrasonication
218 breaks the weak bonding and further disintegrate the fibers into well-dispersed nanofibers. The
219 FESEM image also reveals that the silk nanofibers have been successfully synthesized with
220 widths of a few hundred nanometres and contour lengths of 500-1000 nanometres (Fig. 1c). To
221 detect the topology and quantify the dimension of synthesized nanofibers, AFM is employed
222 by probing the surface of silica wafer with immobilized silk nanofibers. As shown in Fig. 1d,
223 the diameter of the nanofiber is measured to be approximately 20 nm from the depth profile,
224 which aligns well with the diameters of single nanofibers found in natural silks (10-30 nm) [33,
225 34].

226

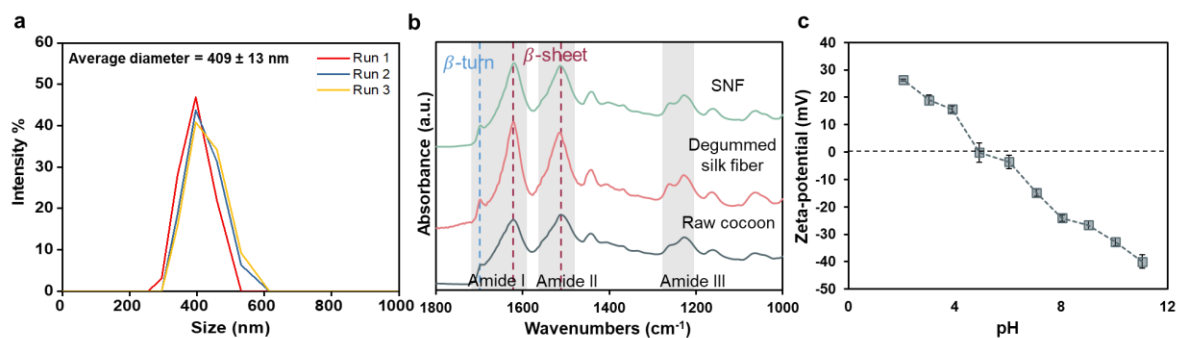
227 To study the size distribution of the prepared SNFs, dynamic light scattering was employed to
228 measure the hydrodynamic diameter of the SNFs. As shown in Fig. 2a, the size distribution
229 curve of the prepared SNF ranges from 300 nm to 600 nm with a centre at 400 nm. The average
230 hydrodynamic diameter of the prepared SNF is 409 ± 13 nm from three experimental runs.
231 This value is substantially greater than the diameter of SNF determined from AFM, as the
232 contour length of the SNF is much larger than the diameter of SNF. In addition, the
233 hydrodynamic diameter of a particle is defined as the diameter of a sphere that exhibits the
234 translational diffusion speed as the particle of interest. It is generally larger than the size of
235 particle measured from SEM or AFM due to the presence of hydrated water molecules and
236 interactions [35, 36]. Nevertheless, the hydrodynamic diameter can reflect the SNF size
237 distribution and dispersity in water.

238

239 The chemistry of silk fibers and possible chemical modification occurred during the synthesis
240 were investigated. The raw cocoon, degummed silk fibers and the obtained SNF were analyzed
241 using FTIR. As shown in Fig. 2b, the strong peaks (1510 and 1618 cm^{-1}) and weak peak (1695
242 cm^{-1}) located in amide I and II band region are assigned to β -sheets and β -turns of hairpin-
243 folded antiparallel β -sheet structure, respectively [37, 38]. This indicates that the silk fibers
244 mainly consist of stable β -sheet structure with strong hydrogen bonds and van der waals forces.
245 In addition, two minor peaks (1220 cm^{-1} and 1261 cm^{-1}) appear at amide III region, which
246 indicates the existence of coil structure. This demonstrates that the silk fibers mainly contain
247 abundant β -sheet structure with a few random coil conformations, as illustrated in Fig. S2.
248 Moreover, the FTIR spectra of the raw cocoon, degummed silk fiber and as synthesized SNF
249 show identical peaks, implying that there is no chemical modification during the degumming
250 and DES dissolution processes. This confirms that the degumming and DES dissolution
251 processing will not destroy the natural properties of the silk fiber.

252

253 Furthermore, the surface charge of the SNFs was characterized by measuring the zeta-potential
254 of SNF aqueous dispersion at different pH conditions. The results show that the zeta-potential
255 of SNF decreases as the pH of SNF dispersion increases, which is due to the complex chemistry
256 of silk fibroin containing various amino acids. The isoelectric point of synthesized SNFs in
257 water is determined to be 4.9, where the surface charge of SNF is neutral. When the pH is
258 below 4.9, the SNFs are positively charged with compacted structures. If the pH increases
259 beyond 4.9, the SNFs become negatively charged, leading to repulsive forces that compel the
260 polypeptide to assume elongated conformations [39, 40]. Therefore, in this study, the pH of as-
261 synthesized SNF dispersion is adjusted to 8 in order to minimize the aggregation of SNFs.



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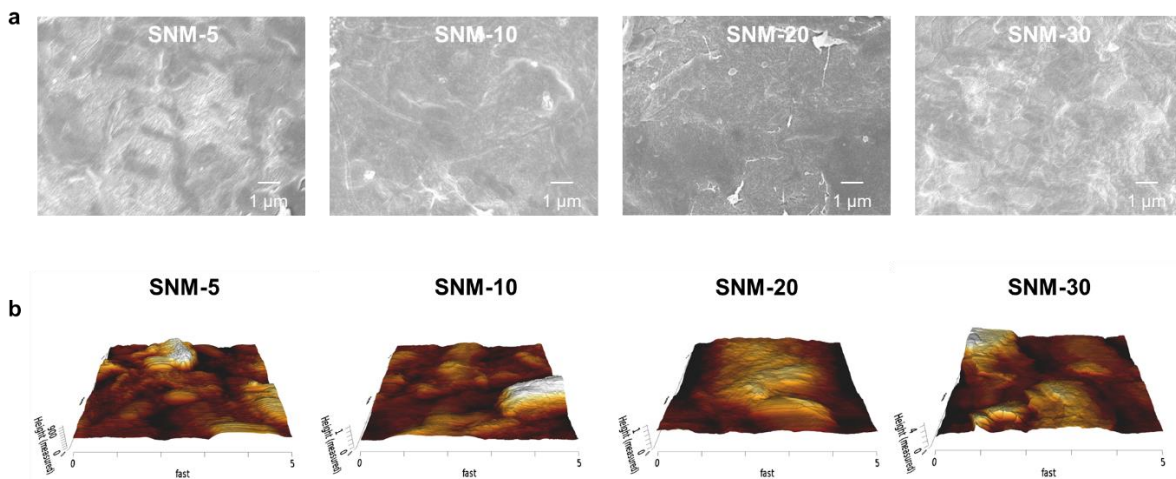
263 **Figure 2 Characterizations of the prepared SNFs.** a) Hydrodynamic diameter distribution
264 and the average diameter of SNFs. b) FTIR spectra of raw cocoon, degummed silk fiber and
265 SNF. c) Surface zeta-potential of SNFs at different pH conditions.

266

267 3.3 Fabrication and characterization of SNF membranes

268 The SNF membrane was assembled by depositing the as-prepared aqueous SNF dispersion on
269 a dopamine coated cellulose acetate membrane substrate via a pressure-assisted self-
270 assembling method. This method is straightforward and environmentally friendly, devoid of
271 the inclusion of harmful chemicals. The SNFs can be firmly attached to the substrate due to the
272 good adhesion property of dopamine and possible hydrogen bonding formed between SNF and

273 cellulose acetate [41, 42]. Different SNF loadings ranging from 20.8 to 124.7 g m⁻² were
274 deposited onto the substrate and investigated. The membrane morphologies of the prepared
275 SNM-5, SNM-10, SNM-20 and SNM-30 were observed using FESEM and AFM, as shown in
276 Fig. 3a and b, respectively. All the membranes possess uniform surfaces with fibrous structures.
277 The nanofiber morphology can be observed on the surface of membranes, especially on the
278 highly loaded ones. From AFM images, rod-like shape SNFs can be observed on the membrane
279 surface. The membrane surfaces are relatively smooth at low SNF loading but become rough
280 when the SNF loading is increased to 124.7 g m⁻². The surface roughness of the prepared
281 membranes is measured at 3 spots and the averaged value is tabulated in Table 1. The root-
282 mean-square (RMS) roughness (R_q) increases slightly from 108.7 to 196.5 nm when the loading
283 increases from 20.8 to 83.2 g m⁻², but it dramatically increases to 638 nm when the loading
284 reaches 124.7 g m⁻². This is probably due to the self-assembly of SNFs during the deposition
285 process, which is driven by thermodynamics and kinetics as explained in the later section.



286

287 **Figure 3 Surface morphologies of fabricated silk nanofiber composite membranes with**
288 **different SNF loadings.** a) FESEM images and b) AFM mappings of SNM-5, SNM-
289 20 and SNM-30 (from left to right).

290

291

292 **Table 1** The SNF loading, thickness and surface roughness of prepared SNMs.

Membrane	Silk nanofiber loading (g/m ²)	Selective layer thickness (μm)	Average roughness (Ra)	RMS roughness (Rq)
SNM-5	20.8	4.8 ± 0.4	78.5 ± 3.3	108.7 ± 4.5
SNM-10	41.6	12.7 ± 0.3	124.3 ± 3.7	158.6 ± 7.2
SNM-20	83.2	37.0 ± 1.0	157.3 ± 6.5	196.5 ± 14.7
SNM-30	124.7	156.1 ± 2.5	517.1 ± 49.3	637.9 ± 16.4

293

294 The thickness of the SNF layer is measured from the cross-section images (Fig. S3) and the

295 values are tabulated in Table 1. The thickness of the SNF layer increases with the loading of

296 SNF; however, the thickness increases linearly from 4.8 to 37.0 μm at low SNF loading and it

297 dramatically increases to 156.1 μm when the SNF loading increases further to 124.7 g m⁻² (Fig.

298 4a and Table 1). In addition, as observed from the cross-sectional images, SNM-5 and 10

299 possessed uniform and dense cross-sections. In comparison, the cross-sections of SNM-20 and

300 30 exhibit a nanofibrous structure, and particularly nanofibrils is observed from the cross-

301 section of SNM-30. The sharp increase of thickness and different morphology can be attributed

302 to the self-assembly and stacking behaviours of SNFs during the deposition process. The self-

303 assembly of SNFs in aqueous dispersion will experience conformation transitions and

304 nanostructure assembly, which is affected by molecular mobility, charge, hydrophilic

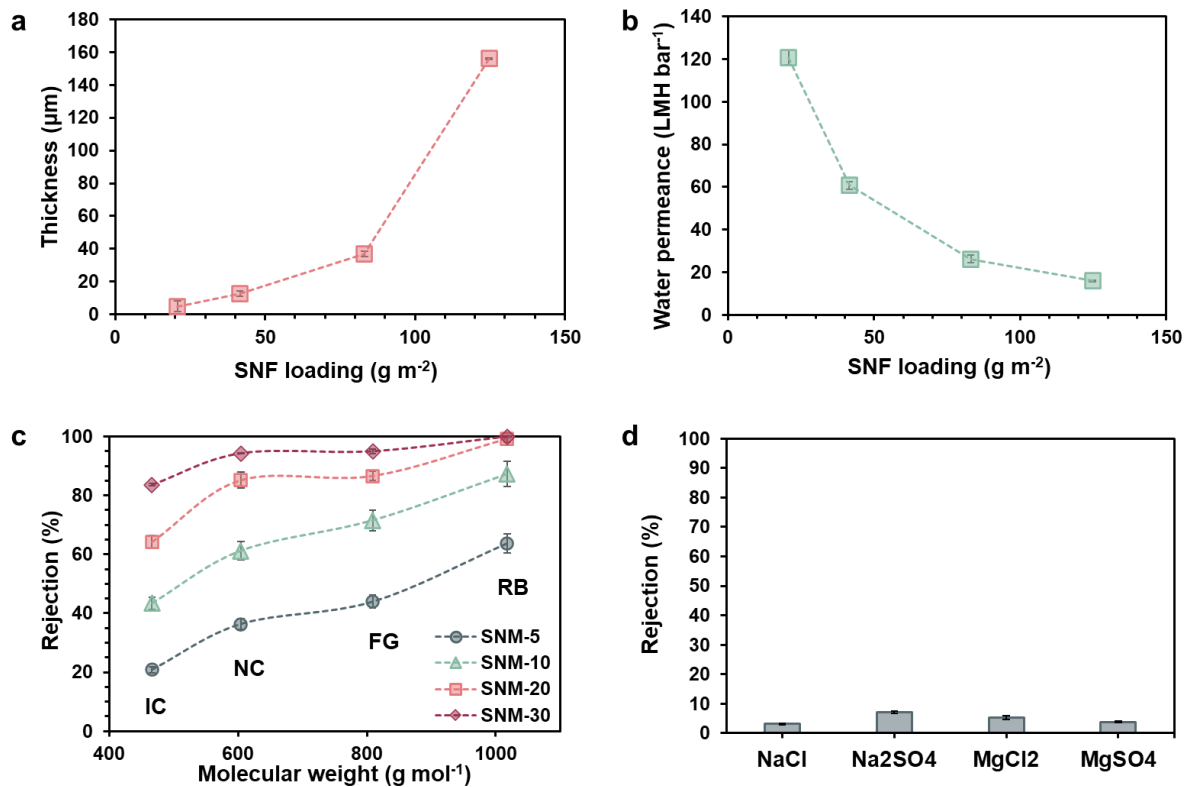
305 interactions, and concentration [39]. As aforementioned, the isoelectric point of SNF is

306 determined to be 4.9, so it exhibits negative surface charge in the prepared dispersion for

307 deposition. Previous studies reported that SNFs would first assemble into micelles and

308 aggregate into nanofibrils especially under high concentrations because of the reduced

309 repulsive forces compared to larger repulsive forces in the case of globule formation [39, 40,
 310 43]. During the deposition process, water will be filtered away slowly, leading to a concentrated
 311 SNF dispersion on top of the membrane. In such manner, SNFs tend to assemble into
 312 nanofibrils at high loading conditions, resulting in a nanofibrous structure that exhibits
 313 increased thickness and surface roughness.



314

315 **Figure 4 Water permeance and separation performance of the silk nanofiber membrane.**

316 a) The relationship between the thickness and SNF loading. b) Water permeances of the silk
 317 nanofiber membranes with different SNF loadings. c) Dye rejections of silk nanofiber
 318 membranes versus the molecular weights of various dyes. IC: Indigo carmine; NC: New
 319 coccine; FG: Fast green FCF; RB: Rose bengal. d) Salt rejections of SNM-20.

320

321 3.4 Separation performance for dye/salt fractionation

322 To investigate the effect of SNF loading on the separation performance of the prepared SNF
 323 composite membranes, water permeances and rejections towards various dyes were measured

324 using SNM-5, 10, 20 and 30. Surprisingly, the SNM-5 exhibits a water permeance of 121 LMH
325 bar^{-1} , which significantly decreases to 26 LMH bar^{-1} when the SNF loading increases to 83.2 g
326 m^{-2} (Fig. 4b). Nevertheless, the rate of decrease in water permeance can be seen to gradually
327 decline when the SNF loading is further increased to 124.7 g m^{-2} . The decrease in water
328 permeance can be ascribed to 1) the increase in the thickness of SNF layer and 2) the densely
329 packed structure of SNF. As aforementioned, the thickness of SNF layer increases linearly at
330 low SNF loading range and rises dramatically when the SNF loading reaches 124.7 g m^{-2} .
331 However, the effect of SNF loading on water permeance deviates from that on membrane
332 thickness, mainly because of the packing structure of SNF on the substrate at different loading
333 conditions. From the cross-sections, SNFs are stacked into a thin and densely packed structure
334 at low SNF loading; as the loading increases, SNFs tend to aggregate and form into a loosely
335 packed nanofibrous structure. Therefore, although the thickness of SNF layer increases
336 significantly at high SNF loading, the water permeance does not decrease significantly because
337 of the loosely packed SNF layer.

338

339 To evaluate the separation efficiency of the SNF composite membranes, various dyes,
340 including indigo carmine (IC), new coccine (NC), fast green FCF (FG) and rose bengal (RB),
341 were employed for filtration tests. Table S1 summarizes the properties and molecular structures
342 of the selected dyes. The rejections of SNF composite membranes with different loadings are
343 measured and reported in Fig. 4c. The rejections of the selected four dyes increases with their
344 molecular weights for all the SNF membranes due to the size-exclusion effect. For instance,
345 the rejection towards IC (MW= 466.4 g mol^{-1}) and RB (MW= 1017.6 g mol^{-1}) of SNM-20 is
346 64% and 99%, respectively. Moreover, the dye rejections increase with the loading of SNFs
347 especially for small molecular dyes, i.e., IC and NC. This is in accordance with the water
348 permeance, as the mass transfer resistance of the membrane increases with the SNF loading.

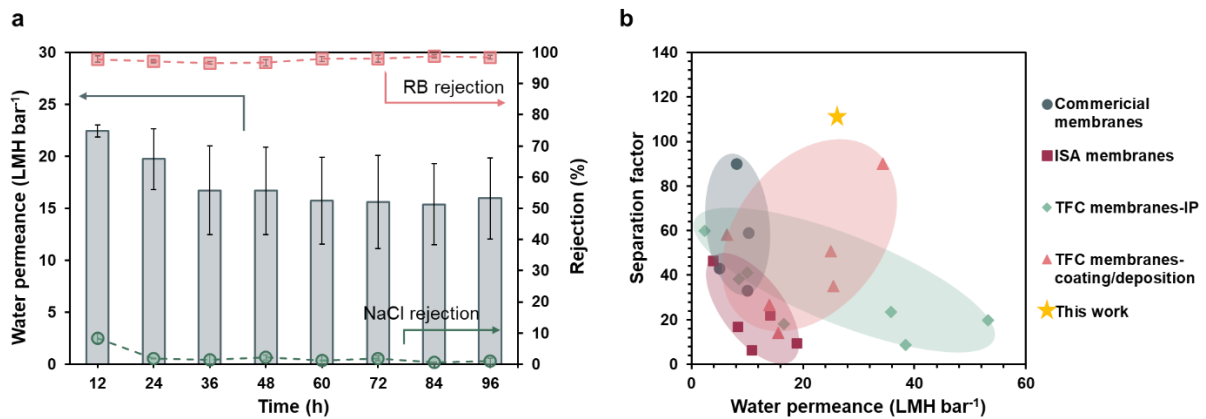
349 Among the four prepared membranes, SNM-20 has relatively high water permeance of 26
350 LMH bar⁻¹ and satisfactory rejections towards dyes. Thus, it is selected for further dye/salt
351 fractionation tests. Prior to dye/salt fractionation test, single salt rejection was measured using
352 1000 ppm of NaCl, Na₂SO₄, MgCl₂ and MgSO₄ solutions as feed solutions at 1 bar. As shown
353 in Fig. 4d, the salt rejections towards these four salts are very low, ranging from 3 % to 7 %,
354 due to the loose structure and large pore size. The low salt rejection and high dye rejection hold
355 significant promise for treating high-salinity wastewater in the textile industry, where high
356 concentrations of NaCl and Na₂SO₄ are commonly employed to improve dye adhesion to
357 fabrics and maximize dye molecule exhaustion [44, 45].

358

359 **3.5 Dye/salt fractionation to treat textile wastewater**

360 In order to study the separation performance and stability of prepared SNF composite
361 membrane in treating textile wastewater, a mixed dye/salt solution containing RB and NaCl
362 was continuously filtrated through the membrane for 100 h. Fig. 5a displays the changes in
363 water permeance and rejection towards NaCl and RB over time. The water permeance
364 experiences a slight decrease within the initial 36 hours, possibly attributable to membrane
365 compaction and fouling phenomena. After the compaction and fouling reach saturation, a stable
366 water permeance is achieved during the test. The rejections towards RB and NaCl remain
367 highly consistent throughout the 100-h test, showcasing excellent stability in the context of
368 textile wastewater separation. The water permeance and separation factor, calculated as the
369 ratio of dye to salt concentration in the permeate to that in the feed, are determined and later
370 compared with membranes reported in literature (Fig. 5b and Table S2). The separation factor
371 of SNF composite membrane in separating rose bengal and NaCl is calculated to be 110.7. The
372 separation factor indicates the membrane's efficiency in separating dyes and salts in a mixed
373 solution. A higher separation factor signifies enhanced performance in separating dye and salt

374 mixtures, an important evaluator that is particularly advantageous for textile wastewater
 375 treatment. Compared with the conventional petroleum-based membranes, the newly developed
 376 biobased SNF composite membrane exhibits outstanding fractionation capabilities between
 377 dyes and salts, surpassing or at least matching the performance of most nanofiltration and
 378 ultrafiltration membranes documented in the literature (Fig. 5b).



379
 380 **Figure 5** a) Continuous dye/salt fractionation test of SNM-20 in rose bengal/NaCl mixture for
 381 100 h. b) Comparison of separation performance with reported membranes in the literature for
 382 dye/salt fractionation.

383

384 3.6 Sustainability evaluation

385 The SNF composite membrane designed in this study employed sustainable materials and
 386 green solvents from the macroscale to the nanoscale. Biobased polymers, SNFs and cellulose
 387 acetate, were used as the selective layer and support, respectively. The SNFs was extracted by
 388 a green DES, which can be recycled and reused for subsequent extraction of SNFs. Cellulose
 389 acetate, sourced from the renewable and abundant cellulose, possesses biodegradability, low
 390 toxicity, chemical stability, mechanical strength and cost-effectiveness, rendering it a good
 391 candidate for membrane substrates. Compatibility between the support and the selective layer
 392 was reinforced by depositing an interlayer using an aqueous solution of polydopamine, sourced
 393 from mussels, known for its good adhesion and biocompatibility. In addition, no organic

394 solvents were used and only water is employed as the processing medium from silkworms to
395 SNF membranes. This is the first reported biobased membrane that does not consist of any
396 petroleum-based materials for dye/salt fractionation. To compare the sustainability of the
397 newly developed biobased SNF membrane with conventional TFC membranes for dye/salt
398 fractionation, the chemicals in the selective layer were listed and their sustainability were
399 evaluated by the hazard and toxicity as indicated by the Globally Harmonized System of
400 Classification and Labelling of Chemicals. As elaborated in [Table S3](#), TFC membranes
401 fabricated by interfacial polymerization and coating often involves health hazard,
402 environmental hazard or toxic compounds, such as trimesoyl chloride, piperazine and
403 polyethyleneimine. In addition, the fabrication processes usually involve the usage of
404 flammable and volatile solvents, such as hexane and toluene. Our proposed green SNF
405 membrane utilizes natural silkworms and recyclable DES without additional organic solvents
406 and dangerous chemicals, demonstrating the enhanced sustainability over traditional petroleum
407 based and partially green TFC membranes.

408

409 **4. Conclusions**

410 In summary, we have demonstrated a green and simple approach to prepare SNF composite
411 membranes for dye/salt fractionation with excellent and stable separation performance. SNFs
412 are firstly extracted from natural silkworms by substituting traditional toxic solvents with DES,
413 which can be recycled and reused for further extraction process. The as-harvested SNFs
414 preserves the native structures and chemistry, yet they are able to reduce its size to nano scale.
415 The SNF composite membrane is fabricated by self-assembling of SNF via a pressure-assisted
416 self-assembling method. By tuning the SNF loadings, the thickness of SNF selective layer can
417 be varied with different separation performance. Interestingly, the thickness of SNF selective
418 layer increases linearly with the loading when the loading is less than 100 g m^{-2} . However, the

419 thickness dramatically increases when the loading exceeds due to the formation of loosely
420 packed SNFs nanofibrous structures at high SNF loading, as supported by SEM and water
421 permeance. The optimized SNF composite membrane exhibits a water permeance of 26 LMH
422 bar^{-1} with high rejection of 99% towards rose bengal. Moreover, the developed SNF composite
423 membrane is capable in continuously fractionating dye and salt for 100 h to treat textile
424 wastewater containing high concentrations of dyes and inorganic salts. The membrane
425 demonstrates a stable water permeance with a separation factor of 110.7, which surpasses most
426 ultrafiltration and nanofiltration membranes reported in literature. By utilizing natural resource
427 and green solvent, the SNF composite membrane holds great potential for sustainable water
428 purification and molecular separation to reduce the footprint and minimize the environmental
429 impact.

430

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438 **References**

- 439 [1] Y. Bhatt, K. Ghuman, A. Dhir, Sustainable manufacturing. Bibliometrics and content
440 analysis, *J. Clean. Prod.*, 260 (2020) 120988.
- 441 [2] A. Moldavska, T. Welo, The concept of sustainable manufacturing and its definitions: A
442 content-analysis based literature review, *J. Clean. Prod.*, 166 (2017) 744-755.
- 443 [3] S.P. Nunes, P.Z. Culfaz-Emecen, G.Z. Ramon, T. Visser, G.H. Koops, W. Jin, M. Ulbricht,
444 Thinking the future of membranes: Perspectives for advanced and new membrane materials
445 and manufacturing processes, *J. Membr. Sci.*, 598 (2020) 117761.
- 446 [4] S. Nair K, B. Manu, A. Azhoni, Sustainable treatment of paint industry wastewater: Current
447 techniques and challenges, *J. Environ. Manage.*, 296 (2021) 113105.
- 448 [5] J. Chen, Q. Wang, Z. Hua, G. Du, Research and application of biotechnology in textile
449 industries in China, *Enzyme Microb. Technol.*, 40 (2007) 1651-1655.
- 450 [6] J. Lin, W. Ye, H. Zeng, H. Yang, J. Shen, S. Darvishmanesh, P. Luis, A. Sotto, B. Van der
451 Bruggen, Fractionation of direct dyes and salts in aqueous solution using loose nanofiltration
452 membranes, *J. Membr. Sci.*, 477 (2015) 183-193.
- 453 [7] P. Jin, J. Zheng, Q. Gao, A.K. An, J. Zhu, B. Van der Bruggen, Loose Nanofiltration
454 Membranes for the Treatment of Textile Wastewater: A Review, *J. Membr. Sci. Res.*, 8 (2022).
- 455 [8] S. Guo, Y. Wan, X. Chen, J. Luo, Loose nanofiltration membrane custom-tailored for
456 resource recovery, *Chem. Eng. J.*, 409 (2021) 127376.
- 457 [9] X. Feng, D. Peng, J. Zhu, Y. Wang, Y. Zhang, Recent advances of loose nanofiltration
458 membranes for dye/salt separation, *Sep. Purifi. Technol.*, 285 (2022) 120228.
- 459 [10] A.W. Mohammad, Y.H. Teow, W.L. Ang, Y.T. Chung, D.L. Oatley-Radcliffe, N. Hilal,
460 Nanofiltration membranes review: Recent advances and future prospects, *Desalination*, 356
461 (2015) 226-254.

462 [11] G.M. Shi, Y. Feng, B. Li, H.M. Tham, J.-Y. Lai, T.S. Chung, Recent progress of organic
463 solvent nanofiltration membranes, *Prog. Polym. Sci.*, 123 (2021) 101470.

464 [12] X.Q. Cheng, Z.X. Wang, X. Jiang, T. Li, C.H. Lau, Z. Guo, J. Ma, L. Shao, Towards
465 sustainable ultrafast molecular-separation membranes: From conventional polymers to
466 emerging materials, *Prog. Mater. Sci.*, 92 (2018) 258-283.

467 [13] W. Xie, T. Li, A. Tiraferri, E. Drioli, A. Figoli, J.C. Crittenden, B. Liu, Toward the next
468 generation of sustainable membranes from green chemistry principles, *ACS Sustainable Chem.*
469 *Eng.*, 9 (2021) 50-75.

470 [14] D. Zou, S.P. Nunes, I.F.J. Vankelecom, A. Figoli, Y.M. Lee, Recent advances in polymer
471 membranes employing non-toxic solvents and materials, *Green Chem.*, 23 (2021) 9815-9843.

472 [15] B. Li, S. Wang, X.J. Loh, Z. Li, T.S. Chung, Closed-loop recyclable membranes enabled
473 by covalent adaptable networks for water purification, *Proc. Natl. Acad. Sci. U.S.A.*, 120 (2023)
474 e2301009120.

475 [16] S. Wang, N. Wang, D. Kai, B. Li, J. Wu, J.C.C. Yeo, X. Xu, J. Zhu, X.J. Loh, N.
476 Hadjichristidis, Z. Li, In-situ forming dynamic covalently crosslinked nanofibers with one-pot
477 closed-loop recyclability, *Nat. Commun.*, 14 (2023) 1182.

478 [17] B. Li, C. Qu, S. Wang, J.C.C. Yeo, N.E.B. Surat'man, X.J. Loh, Z. Li, T.S. Chung, Closed-
479 loop recyclable dynamic covalent crosslinked nanofibrous membranes for efficient oil/water
480 separation, *J. Membr. Sci.*, 693 (2024) 122378.

481 [18] A. Figoli, T. Marino, S. Simone, E. Di Nicolò, X.M. Li, T. He, S. Tornaghi, E. Drioli,
482 Towards non-toxic solvents for membrane preparation: a review, *Green Chem.*, 16 (2014)
483 4034-4059.

484 [19] X. Jiang, W.F. Yong, J. Gao, D.-D. Shao, S.-P. Sun, Understanding the role of substrates
485 on thin film composite membranes: A green solvent approach with TamiSolve® NxG, *J.*
486 *Membr. Sci.*, 635 (2021) 119530.

487 [20] S.U. Hong, Y. Wang, L.S. Soh, W.F. Yong, Are green solvents truly green? Integrating
488 life cycle assessment and techno-economic analysis for sustainable membrane fabrication,
489 *Green Chem.*, 25 (2023) 4501-4512.

490 [21] L. Sing Soh, S. Uyin Hong, C. Zeng Liang, W. Fen Yong, Green solvent-synthesized
491 polyimide membranes for gas separation: Coupling Hansen solubility parameters and synthesis
492 optimization, *Chem. Eng. J.*, 478 (2023) 147451.

493 [22] F. Galiano, K. Briceño, T. Marino, A. Molino, K.V. Christensen, A. Figoli, Advances in
494 biopolymer-based membrane preparation and applications, *J. Membr. Sci.*, 564 (2018) 562-
495 586.

496 [23] Y. Zhang, X. Cheng, X. Jiang, J.J. Urban, C.H. Lau, S. Liu, L. Shao, Robust natural
497 nanocomposites realizing unprecedented ultrafast precise molecular separations, *Mater. Today*,
498 36 (2020) 40-47.

499 [24] C. Yang, F. Topuz, S.-H. Park, G. Szekely, Biobased thin-film composite membranes
500 comprising priamine–genipin selective layer on nanofibrous biodegradable polylactic acid
501 support for oil and solvent-resistant nanofiltration, *Green Chem.*, 24 (2022) 5291-5303.

502 [25] C. Vepari, D.L. Kaplan, Silk as a biomaterial, *Prog. Polym. Sci.*, 32 (2007) 991-1007.

503 [26] A. Reizabal, C.M. Costa, L. Pérez-Álvarez, J.L. Vilas-Vilela, S. Lanceros-Méndez, Silk
504 Fibroin as Sustainable Advanced Material: Material Properties and Characteristics, Processing,
505 and Applications, *Adv. Funct. Mater.*, 33 (2023) 2210764.

506 [27] Y. Hu, L. Liu, J. Yu, Z. Wang, Y. Fan, Preparation of Natural Multicompatible Silk
507 Nanofibers by Green Deep Eutectic Solvent Treatment, *ACS Sustainable Chem. Eng.*, 8 (2020)
508 4499-4510.

509 [28] W. Xin, Z. Zhang, X. Huang, Y. Hu, T. Zhou, C. Zhu, X.-Y. Kong, L. Jiang, L. Wen,
510 High-performance silk-based hybrid membranes employed for osmotic energy conversion, *Nat.*
511 *Commun.*, 10 (2019) 3876.

512 [29] E.L. Smith, A.P. Abbott, K.S. Ryder, Deep Eutectic Solvents (DESs) and Their
513 Applications, *Chem. Rev.*, 114 (2014) 11060-11082.

514 [30] H.-C. Yang, R.Z. Waldman, M.-B. Wu, J. Hou, L. Chen, S.B. Darling, Z.-K. Xu,
515 Dopamine: Just the Right Medicine for Membranes, *Adv. Funct. Mater.*, 28 (2018) 1705327.

516 [31] B. Li, Y. Cui, S. Japip, Z. Thong, T.S. Chung, Graphene oxide (GO) laminar membranes
517 for concentrating pharmaceuticals and food additives in organic solvents, *Carbon*, 130 (2018)
518 503-514.

519 [32] X. Tan, W. Zhao, T. Mu, Controllable exfoliation of natural silk fibers into nanofibrils by
520 protein denaturant deep eutectic solvent: nanofibrous strategy for multifunctional membranes,
521 *Green Chem.*, 20 (2018) 3625-3633.

522 [33] K. Zheng, J. Zhong, Z. Qi, S. Ling, D.L. Kaplan, Isolation of Silk Mesostructures for
523 Electronic and Environmental Applications, *Adv. Funct. Mater.*, 28 (2018) 1806380.

524 [34] N. Lin, X.Y. Liu, Correlation between hierarchical structure of crystal networks and
525 macroscopic performance of mesoscopic soft materials and engineering principles, *Chem. Soc.*
526 *Rev.*, 44 (2015) 7881-7915.

527 [35] L. Xiao, Z. Ding, X. Zhang, X. Wang, Q. Lu, D.L. Kaplan, Silk Nanocarrier Size
528 Optimization for Enhanced Tumor Cell Penetration and Cytotoxicity In Vitro, *ACS Biomater.*
529 *Sci. Eng.*, 8 (2022) 140-150.

530 [36] H. Fissan, S. Ristig, H. Kaminski, C. Asbach, M. Epple, Comparison of different
531 characterization methods for nanoparticle dispersions before and after aerosolization, *Anal.*
532 *Methods*, 6 (2014) 7324-7334.

533 [37] F. Zhang, Q. Lu, J. Ming, H. Dou, Z. Liu, B. Zuo, M. Qin, F. Li, D.L. Kaplan, X. Zhang,
534 Silk dissolution and regeneration at the nanofibril scale, *J. Mater. Chem. B*, 2 (2014) 3879-
535 3885.

536 [38] C. Guo, J. Zhang, X. Wang, A.T. Nguyen, X.Y. Liu, D.L. Kaplan, Comparative Study of
537 Strain-Dependent Structural Changes of Silkworm Silks: Insight into the Structural Origin of
538 Strain-Stiffening, *Small*, 13 (2017) 1702266.

539 [39] Q. Lu, H. Zhu, C. Zhang, F. Zhang, B. Zhang, D.L. Kaplan, Silk Self-Assembly
540 Mechanisms and Control From Thermodynamics to Kinetics, *Biomacromolecules*, 13 (2012)
541 826-832.

542 [40] J. Zhong, M. Ma, W. Li, J. Zhou, Z. Yan, D. He, Self-assembly of regenerated silk fibroin
543 from random coil nanostructures to antiparallel β -sheet nanostructures, *Biopolymers*, 101
544 (2014) 1181-1192.

545 [41] W. Zhao, S. Cao, H. Cai, Y. Wu, Q. Pan, H. Lin, J. Fang, Y. He, H. Deng, Z. Liu,
546 Chitosan/silk fibroin biomimic scaffolds reinforced by cellulose acetate nanofibers for smooth
547 muscle tissue engineering, *Carbohydr. Polym.*, 298 (2022) 120056.

548 [42] A. Rivera-Galletti, C.R. Gough, F. Kaleem, M. Burch, C. Ratcliffe, P. Lu, D. Salas-de la
549 Cruz, X. Hu, Silk-Cellulose Acetate Biocomposite Materials Regenerated from Ionic Liquid,
550 *Polymers*, 13 (2021).

551 [43] M.A. de Moraes, T. Crouzier, M. Rubner, M.M. Beppu, Factors Controlling the
552 Deposition of Silk Fibroin Nanofibrils during Layer-by-Layer Assembly, *Biomacromolecules*,
553 16 (2015) 97-104.

554 [44] H.-F. Xiao, C.-H. Chu, W.-T. Xu, B.-Z. Chen, X.-H. Ju, W. Xing, S.-P. Sun, Amphibian-
555 inspired amino acid ionic liquid functionalized nanofiltration membranes with high water
556 permeability and ion selectivity for pigment wastewater treatment, *J. Membr. Sci.*, 586 (2019)
557 44-52.

558 [45] J. Zhu, M. Tian, J. Hou, J. Wang, J. Lin, Y. Zhang, J. Liu, B. Van der Bruggen, Surface
559 zwitterionic functionalized graphene oxide for a novel loose nanofiltration membrane, *J. Mater.*
560 *Chem. A*, 4 (2016) 1980-1990.

